

Beyond classical CFD-DEM

# Forgotten Challenges and New Tools

S. RADL

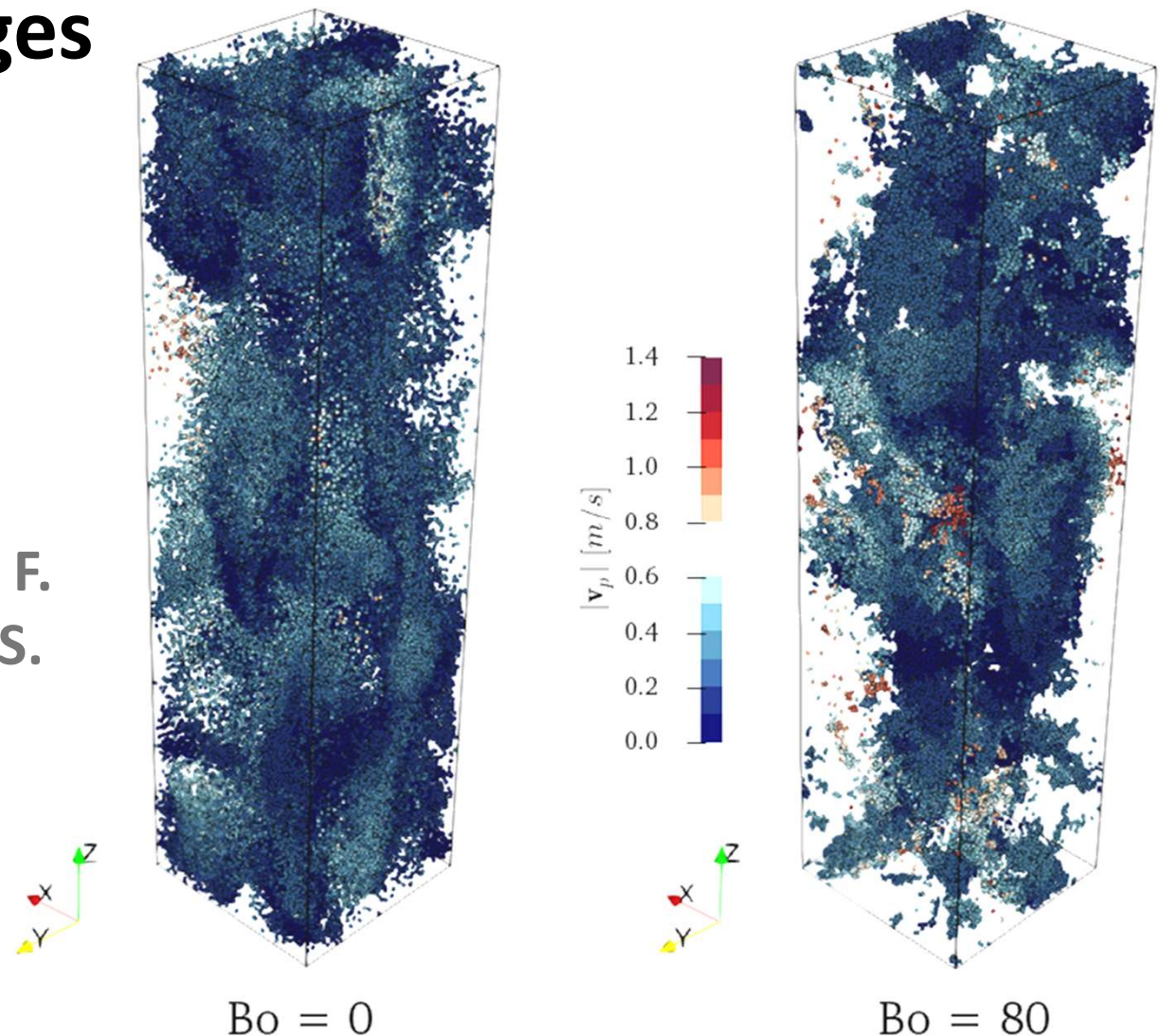
with contributions from

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BENABCHIASLI, N. GHODS, F.  
GOIO CASTRO, M. SALEHI, S.  
SUNDARESAN, & J.  
TAUSENDSCHÖN

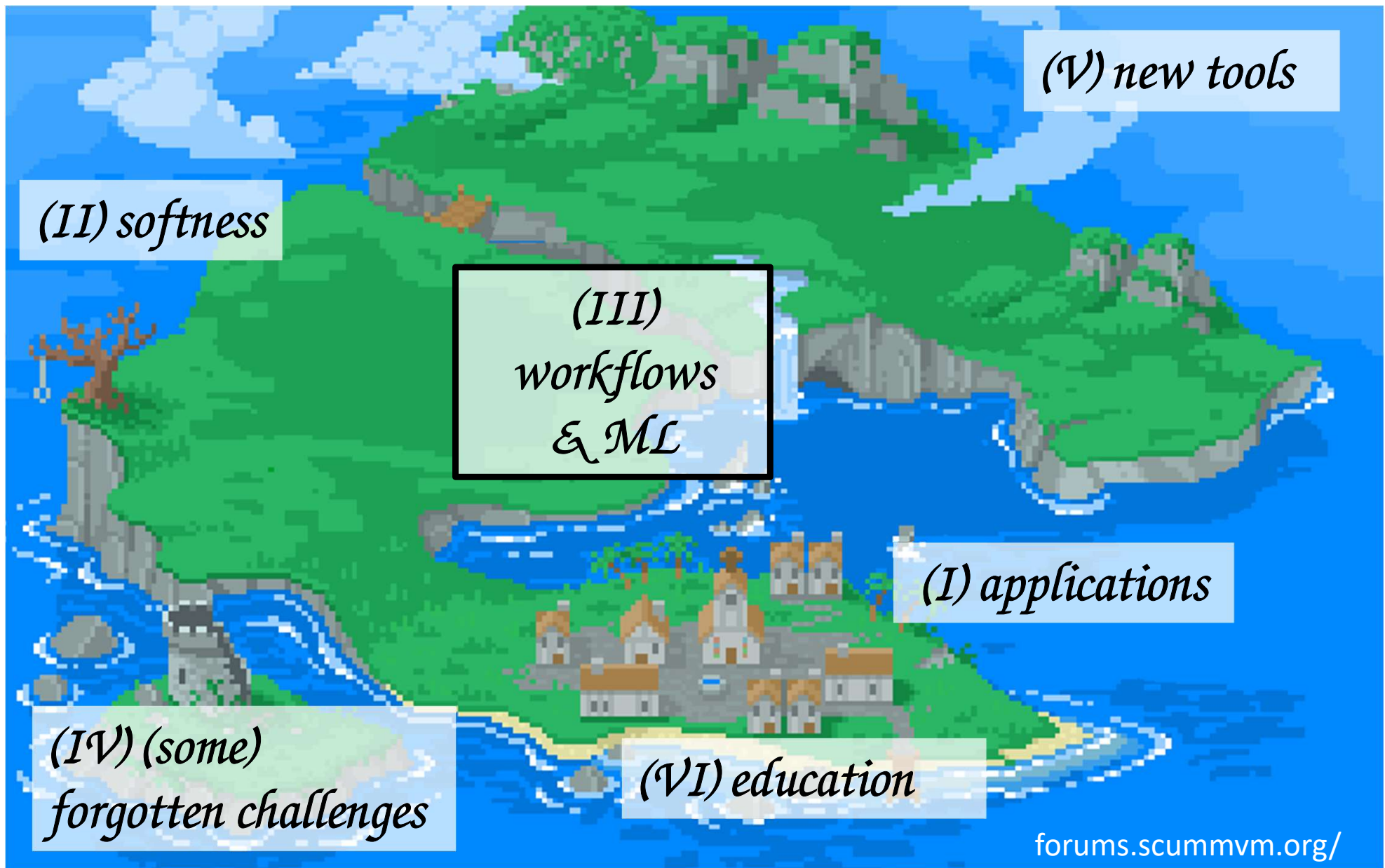
SFB/CRC 287 Retreat

June 13, 2023

Hannover



# Overview





- Batteries I: thermal runaway**

...super fast, super hot and  
supersonic

...tribocharging

...hydrolysis of water vapor

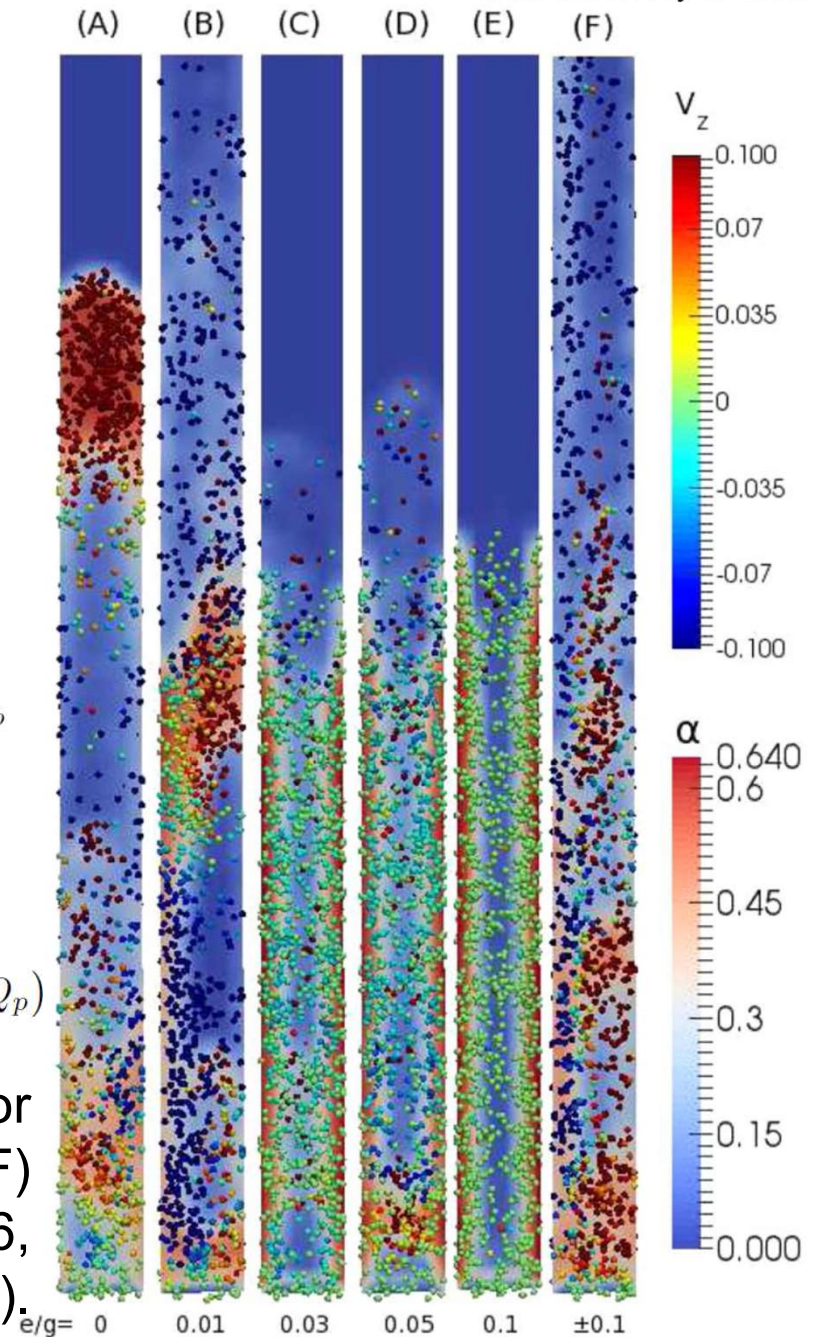
...sparks and arcs

...800V operating voltage

$$\begin{aligned} \frac{3}{2} \frac{\partial}{\partial t} (\alpha_p \rho_p \Theta_p) + \frac{3}{2} \nabla \cdot (\alpha_p \rho_p \Theta_p \mathbf{u}_p) &= \nabla \cdot (\kappa_p \nabla \Theta_p) - (\Sigma_p^{\text{kc}} + \Sigma_p^{\text{fr}}) : \nabla \mathbf{u}_p \\ &\quad - 12 (1 - e_{c,p}^2) \frac{\alpha_p^2 \rho_p g_{0,p}}{d_p \sqrt{\pi}} \Theta_p^{\frac{3}{2}} \\ &\quad - 3\beta \Theta_p, \end{aligned}$$

$$\frac{\partial}{\partial t} \left( \frac{\alpha_p}{V_p} Q_p \right) + \nabla \cdot \left( \frac{\alpha_p}{V_p} Q_p \mathbf{u}_p \right) = \nabla \cdot (\sigma_{q,p} \mathbf{E}) + \nabla \cdot ((\kappa_{q,p} + \kappa_{q,p}^*) \nabla Q_p)$$

Behavior of a fluidized gas-particle system for  
uncharged (A), monopolar (B-E), and bi-polar (F)  
particle charging (Kolehmainen et al., 2016,  
AIChE J.).



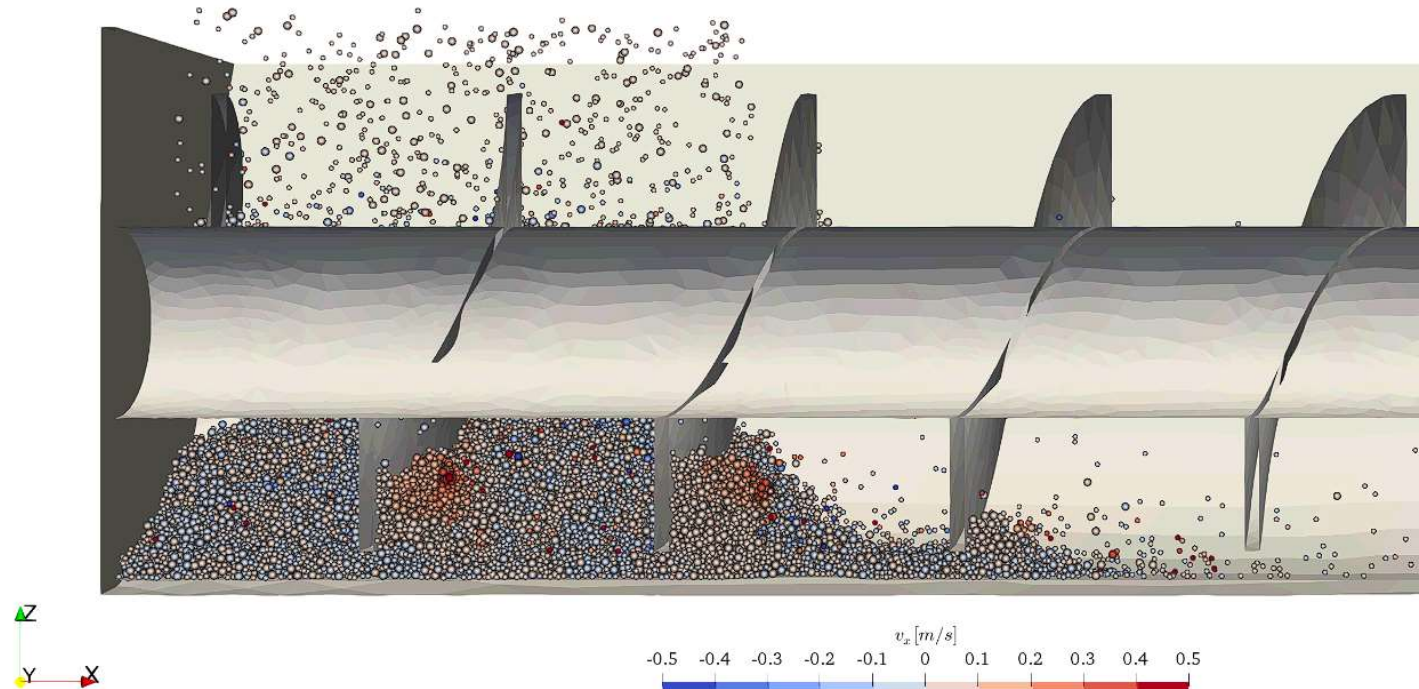
- **Batteries II: recycling**

...keep cool! (because of reactions)

...really complex rheology (wet fibres mixed with small particles) → calibration

...spontaneous carbonation in air (changing rheology)

Cohesive battery  
recyclate flow in a  
screw conveyor  
(Hadie  
Benabchiasli)



- **Wet Granulation**

...fluidization of cohesive  
powders

... spraying & drying

... binders with complex  
rheology



Askarishahi et al.,  
Processes, 2023

Askarishahi et al., Ind. Eng. Chem.  
Res. 61, 2022

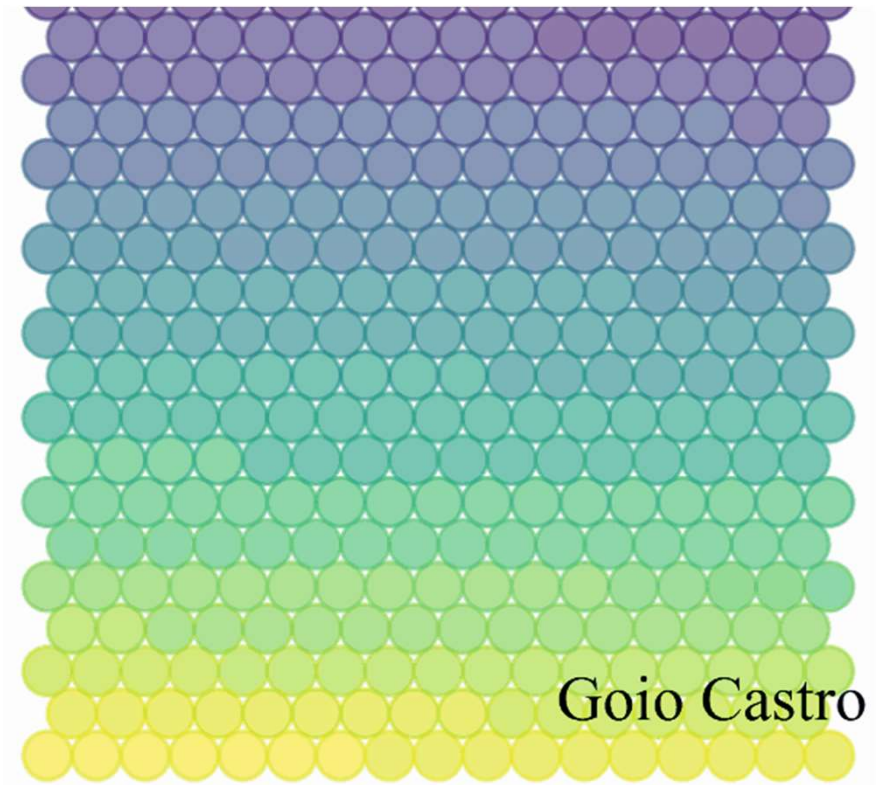
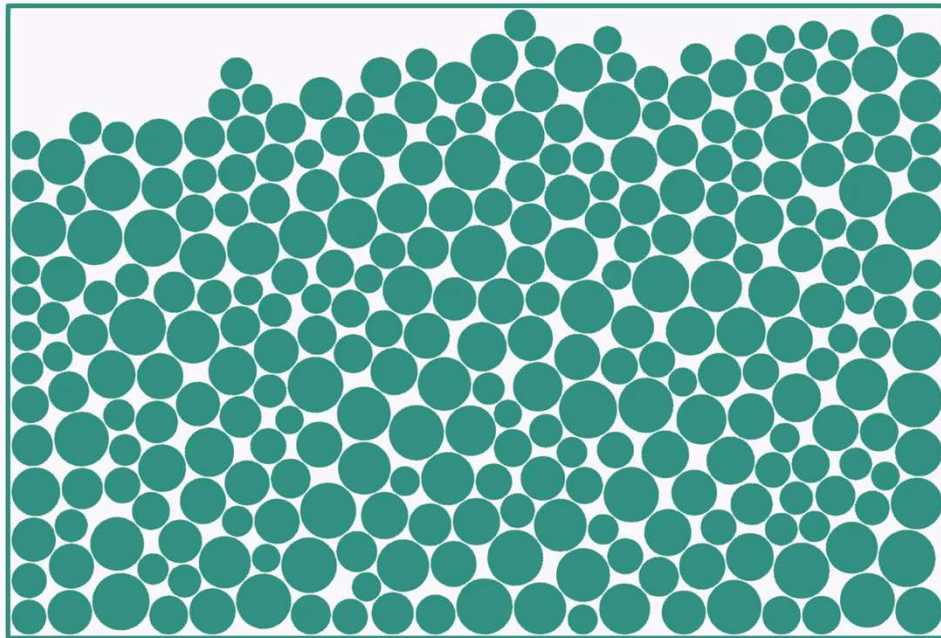


- **Compaction and discharge**

- ...unsteady gas-particle at extreme speed  
(bag filling time  $< 1$  s)

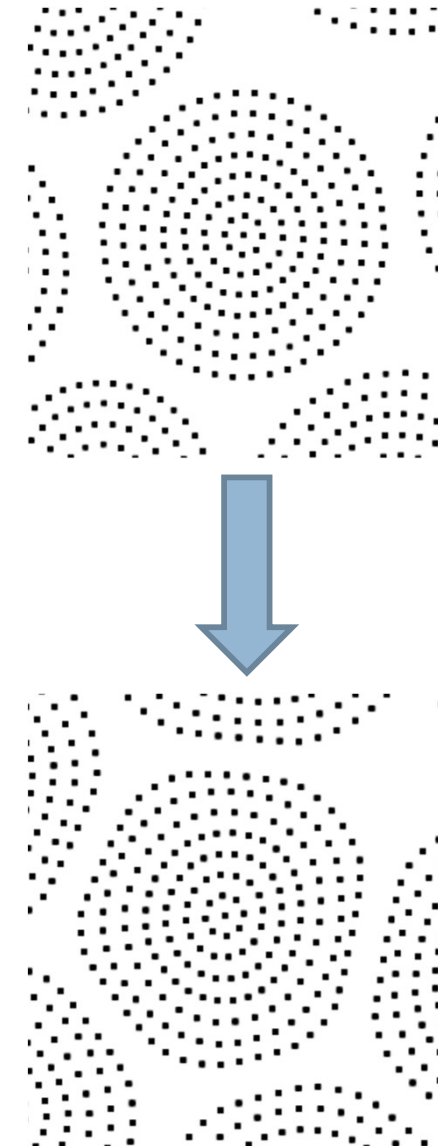
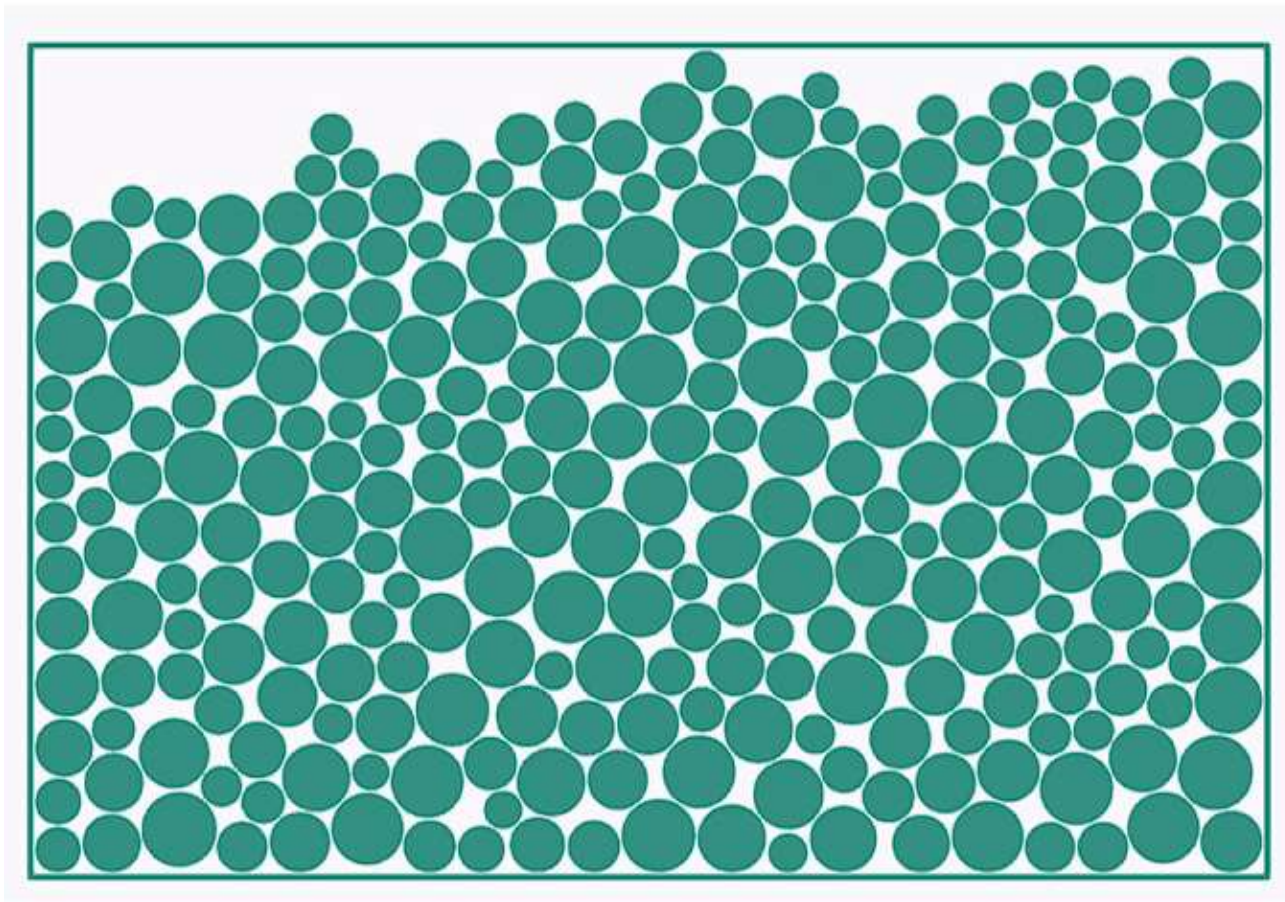
- ...effect of (relative) softness

- ...multi-contact DEM model (“neighbor contact effects”)



SPH-DEM simulation of compaction (left) and silo discharge (right; 2D  
Francisco Goio Castro)

- **Approach I: Resolved Particles with SPH-DEM**



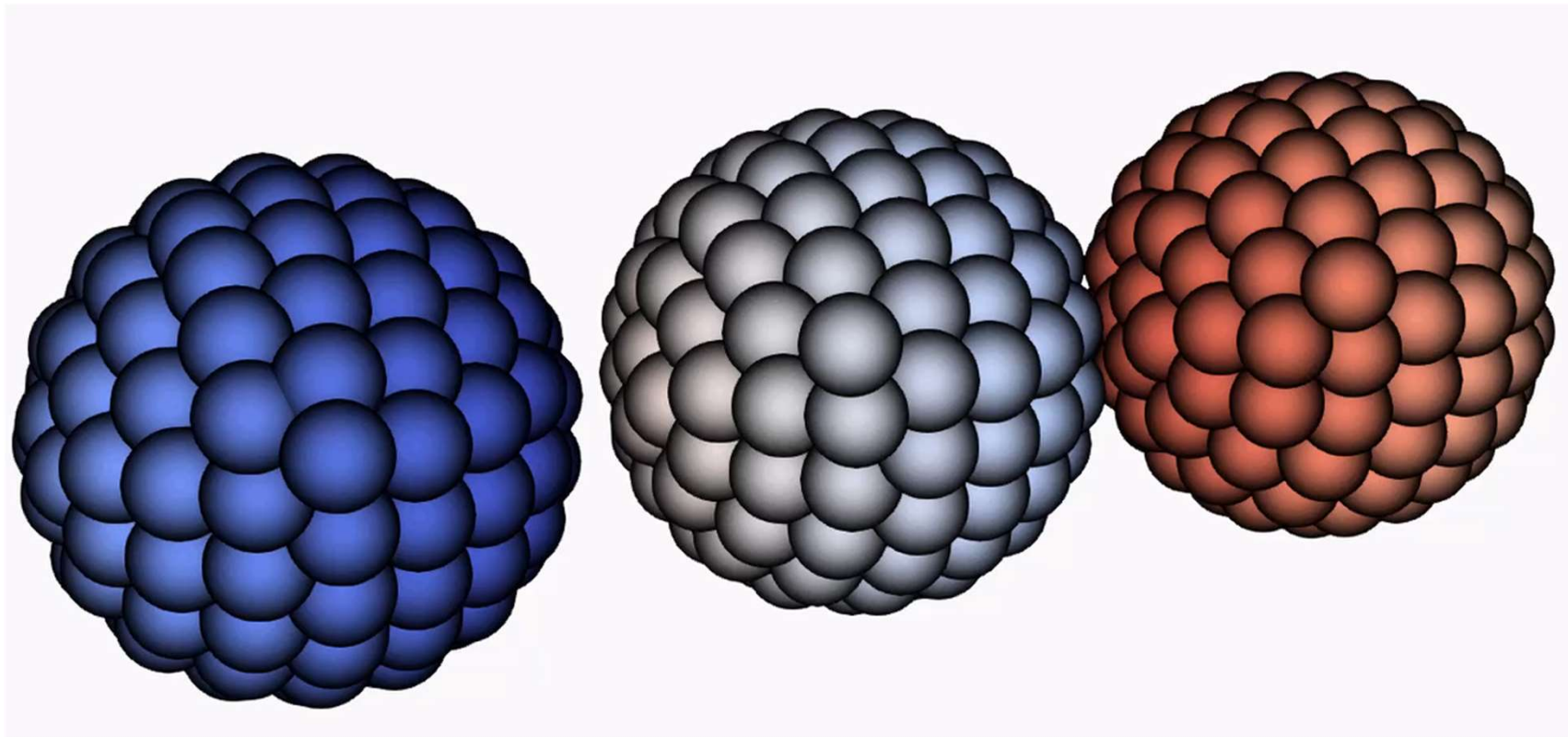
Goio Castro & Radl, Comput Part Mech (accepted)



- **Approach I: Resolved Particles with SPH-DEM**

...SPH for intra-particle deformation

...DEM-type model for inter-particle interactions  
(penalty approach)



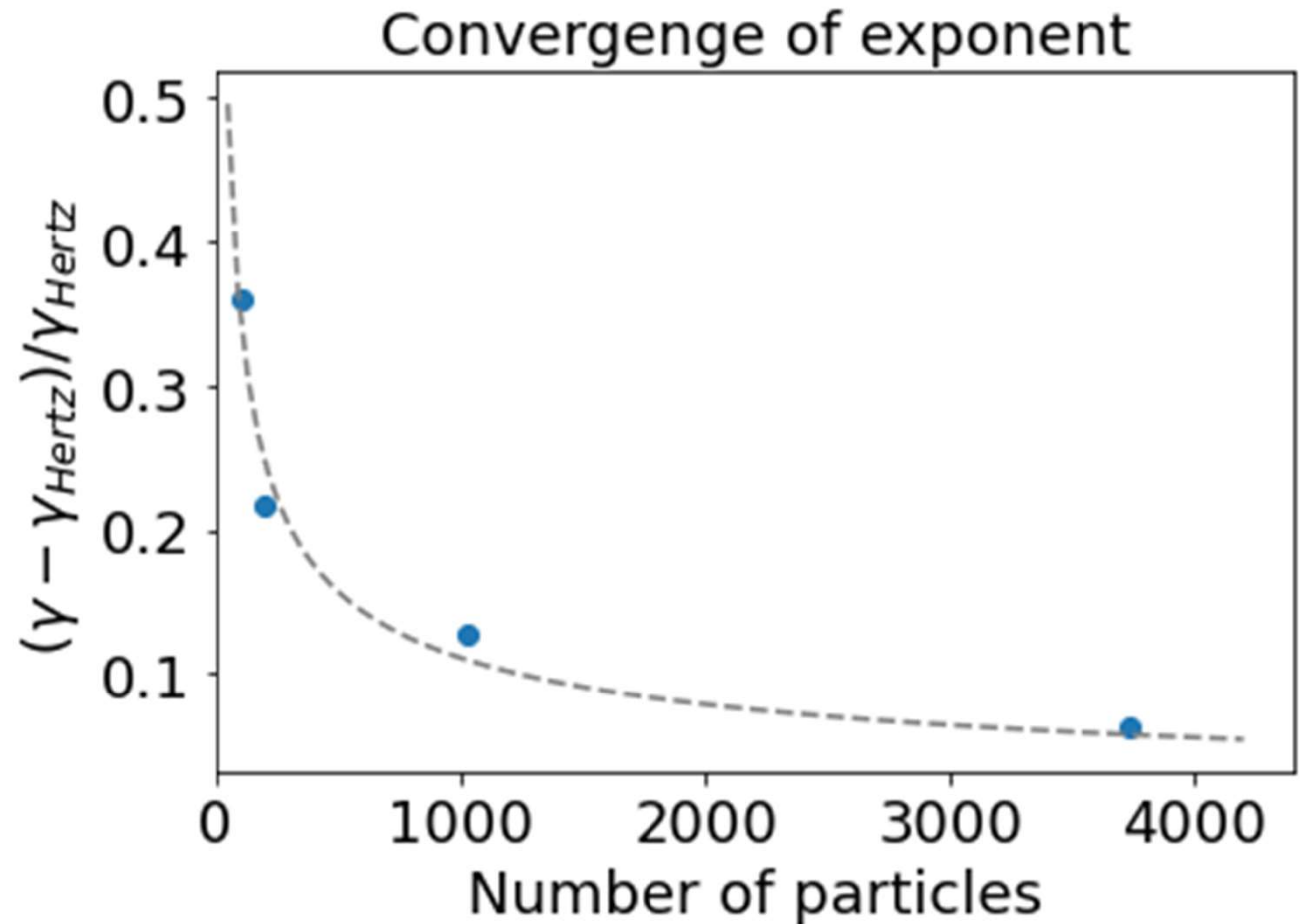


- **Approach I: Resolved Particles with SPH-DEM**

Resolution

Requirements:  
force Exponent  
in overlap  
relation:

$$F_{cont} \propto \delta^\gamma$$



- Approach II: Multi-Contact (MC) Force Closure

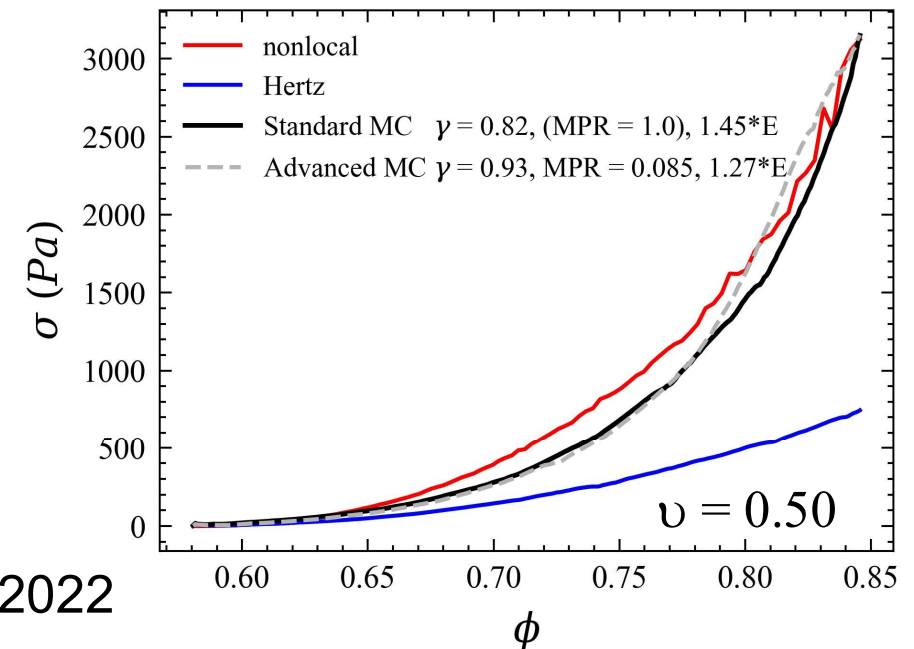
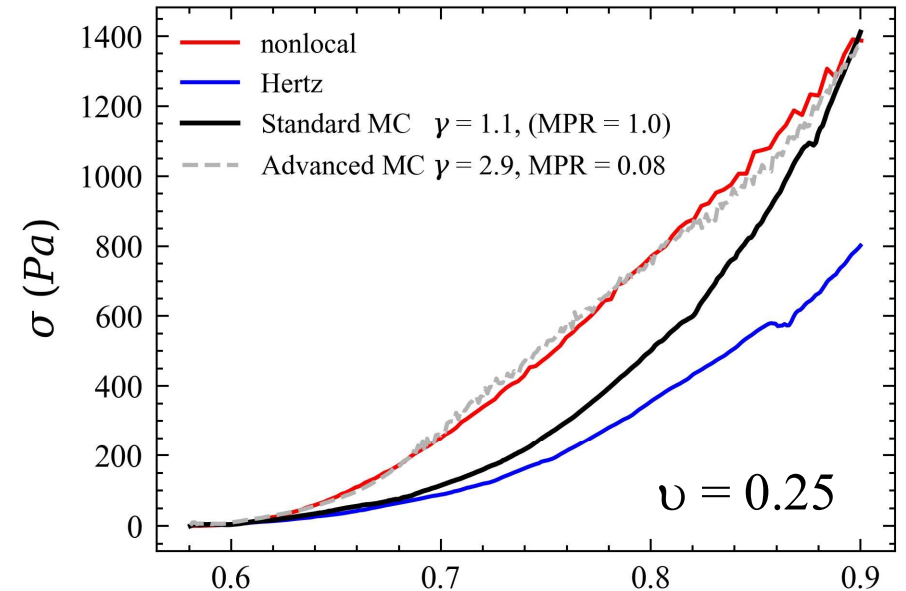
Basics and Benchmarking (Compaction)

$$\delta_c = (r_i + r_j) - (\mathbf{x}_i - \mathbf{x}_j) \cdot \mathbf{n}$$

$$\delta_{k \rightarrow c}$$

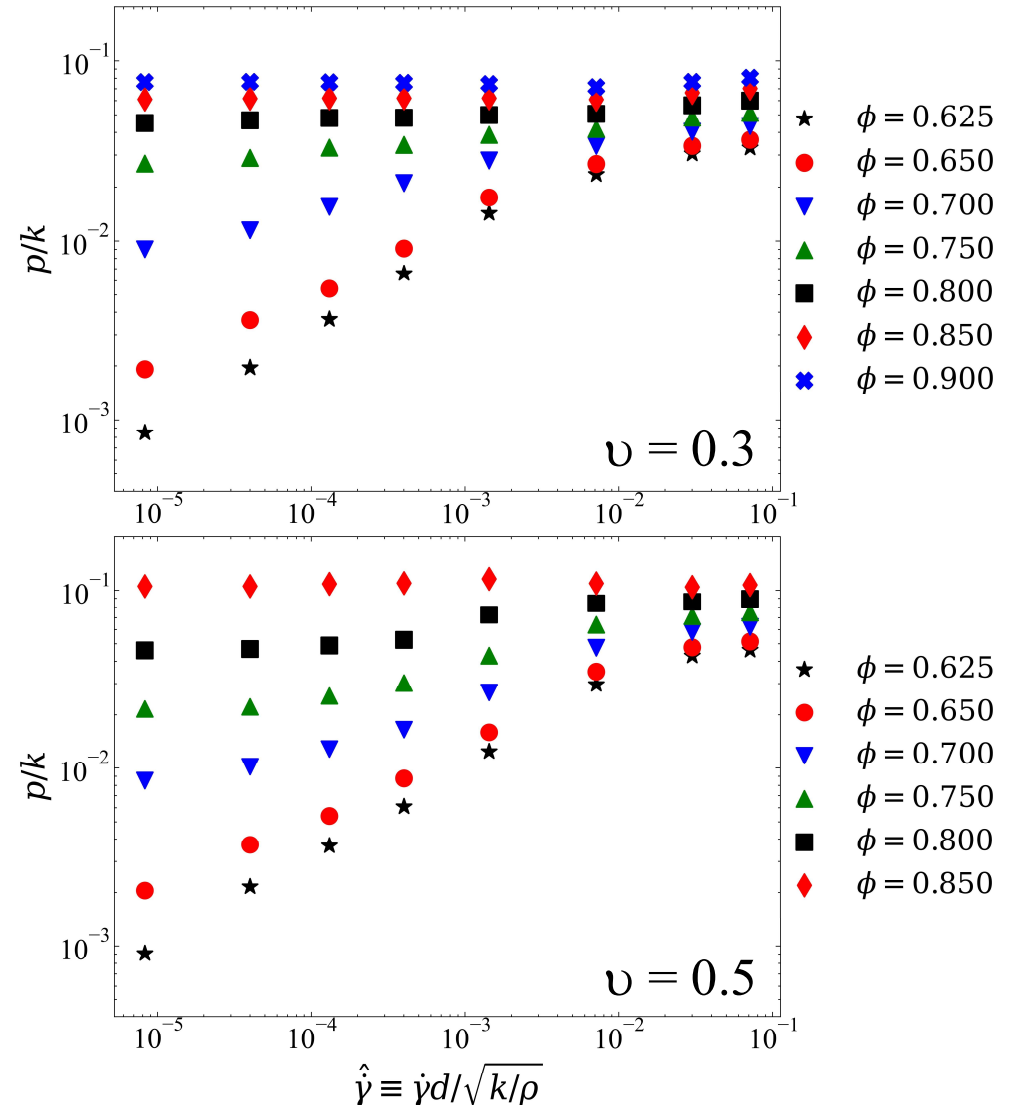
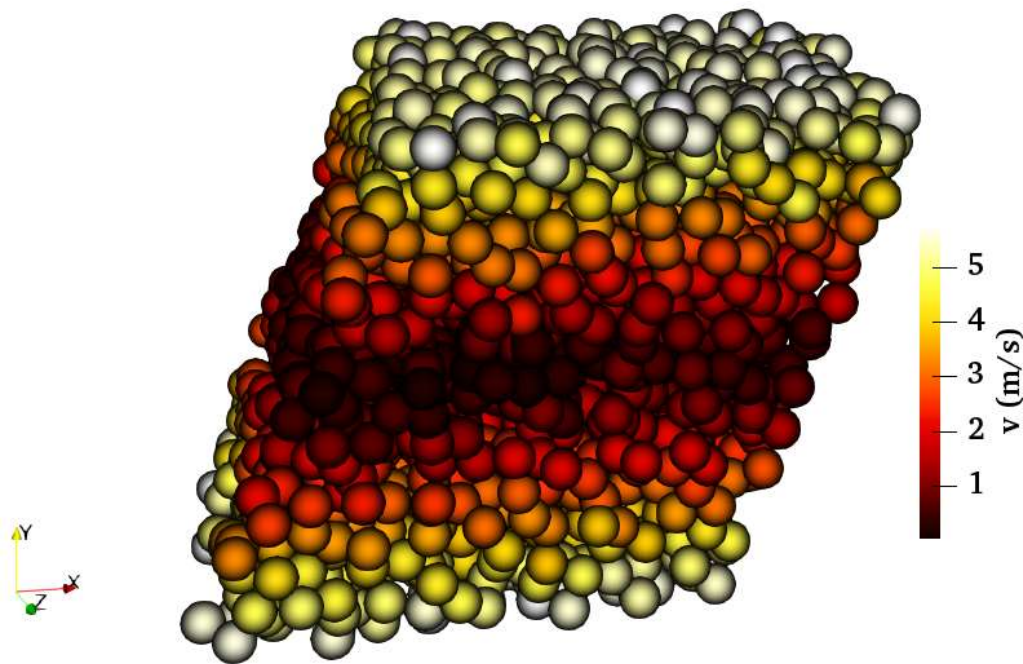
$$= -\gamma \frac{(1 + \nu)F_k}{2\pi E d_{kc}} \left\{ (\mathbf{n}_k \cdot \mathbf{u}_{kc})(\mathbf{n}_c \cdot \mathbf{u}_{kc}) + (3 - 4\nu)\mathbf{n}_k \cdot \mathbf{n}_c - (1 - 2\nu) \frac{(\mathbf{n}_k + \mathbf{u}_{kc}) \cdot \mathbf{n}_c}{1 + \mathbf{n}_k \cdot \mathbf{u}_{kc}} \right\}$$

**+limiter**



- Approach II: Multi-Contact (MC) Force Closure**

Application case: dense shear flow (Lees-Edwards BCs)

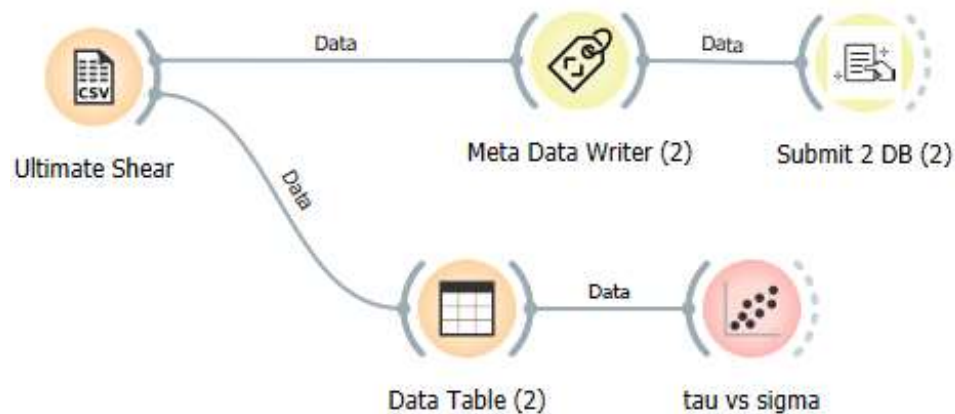




# Overview



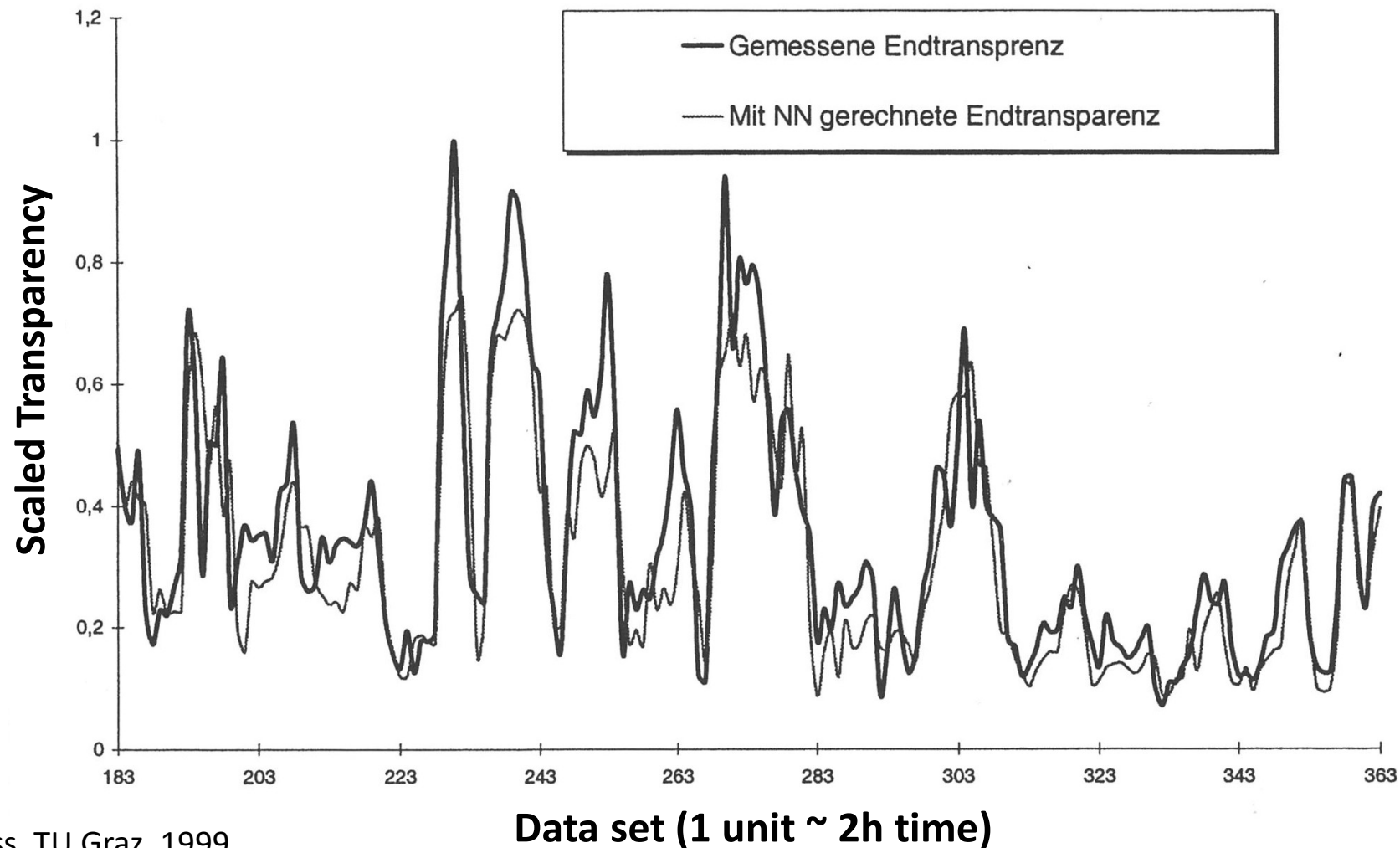
- **From the past...**
  - ...“New” NNs
  - ...via coarse graining
  - ...to anisotropic drag corrections
- **...via the Need 4 Speed...**
- **...to new perspectives**





- “SNNS” is created in 90’s as a tool to make predictions
- Fuchs uses SNNS to predict sedimentation performance of sludge based on training with **182 (!) data points**

“Smart” (ML-based) predictors





- The **need for coarse graining** when simulating suspensions is demonstrated (Agrawal et al, 2001; Radl & Sundaresan, 2014)
- **Refinement of E-L and E-E simulators** and post-processing tools (Capecelatro & Desjardins, 2013)

**Euler-Euler, and  
Euler-Lagrange  
simulators**



Askarishahi et al., Ind. Eng. Chem. Res., 61, 2022.

- **Dedicated tools** for spatial averaging were developed

(Municchi et al., 2016)

for  $A = 0 \rightarrow N_{\text{cells}}$

$$\text{do } \overline{\varphi}_A = \frac{\sum_{n=0}^{n=N_f} \varphi_n}{N_f}$$

endfor

No final step required

$\varphi$ : field to be filtered  
 $A$ : current filtered cell  
 $n$ : neighboring cells

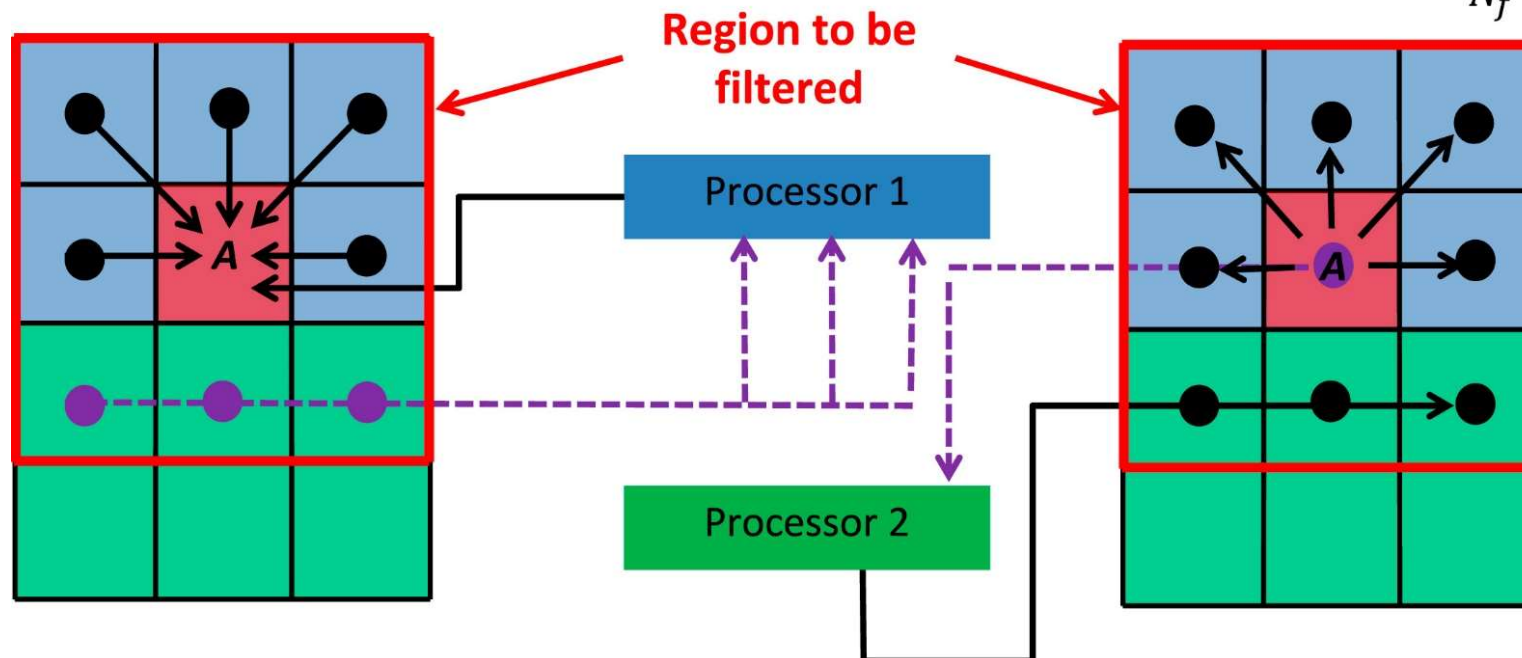
for  $A = 0 \rightarrow N_{\text{cells}}$

do  $\varphi_n += \varphi_A$

endfor

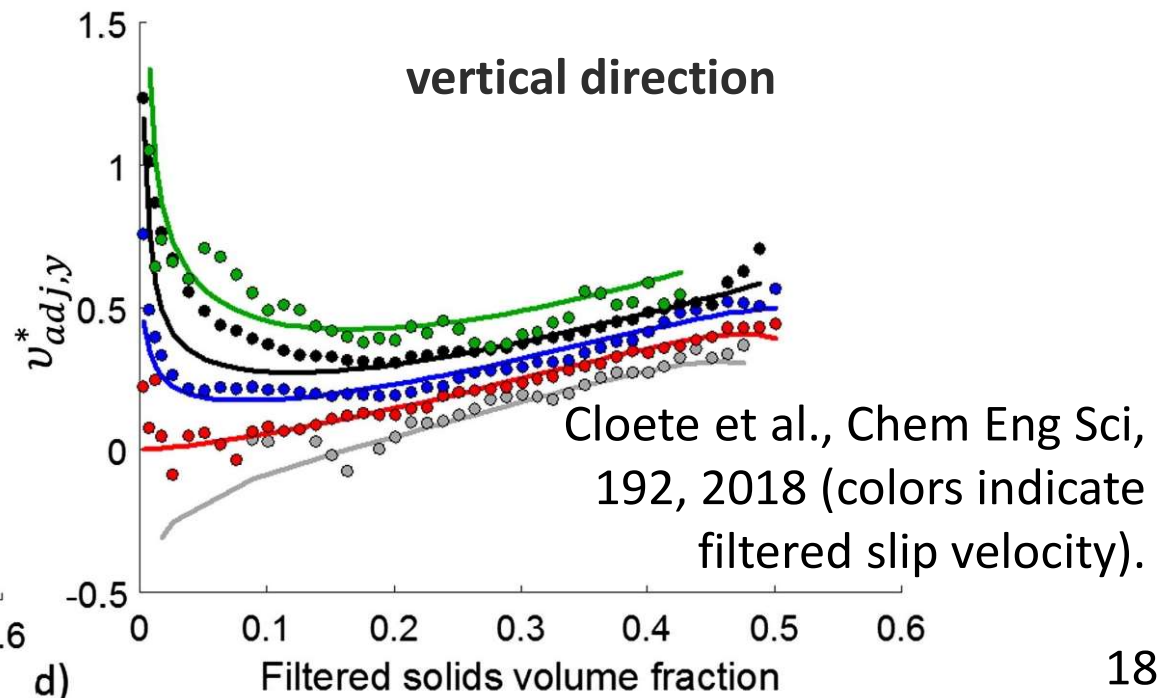
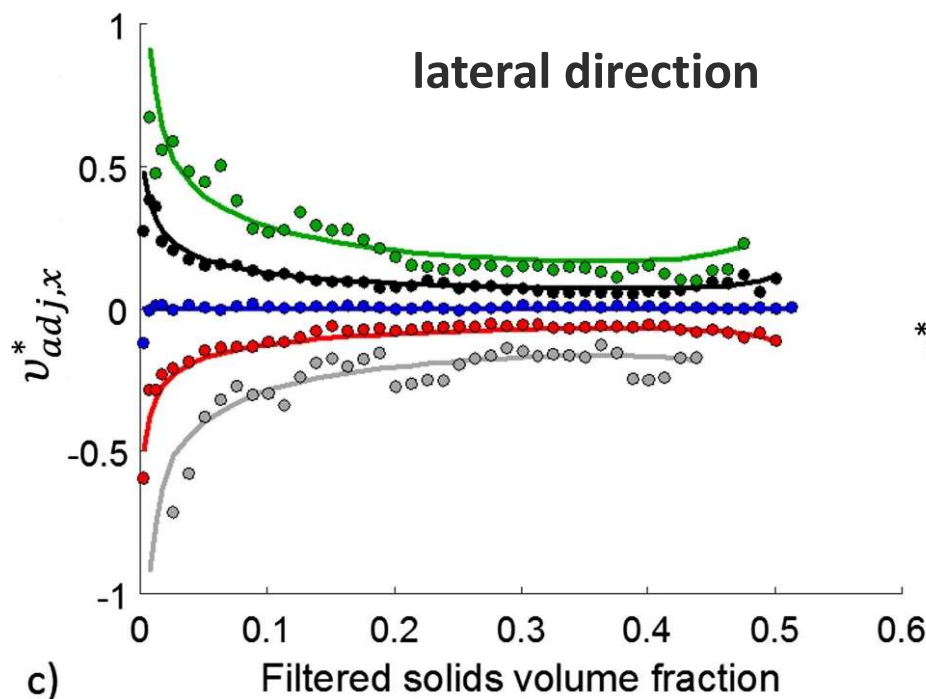
Final step:  $\overline{\varphi}_n = \frac{\varphi_n}{N_f}$

**“Filtering”  
(averaging)  
Tools**



- New families of closure strategies were developed (“**refiltering**” idea of Schneiderbauer and Saeedipour, PoF, 30, 2018)
- ...or modeling is entirely **data-driven** (“**rCFD play back**” approach of Lichtenegger and Pirker, Chem Eng Sci, 153, 2016).
- **Anisotropy** of corrections is (not surprisingly!) identified as a **key need**. This is relevant for **stress and drag** terms!

filtered TFM,  
“fast” CFD, novel  
closures





- Particles which are fine or with **cohesive interactions** (e.g., liquid bridge force) are widely used

Pharmaceuticals



Chemicals



Food



- **Challenges**

- agglomeration and segregation
- blockage & depositions
- inefficient mixing
- Equipment performance <20%

- **Experimental route**

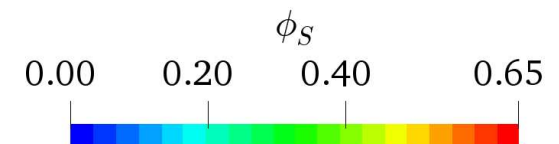
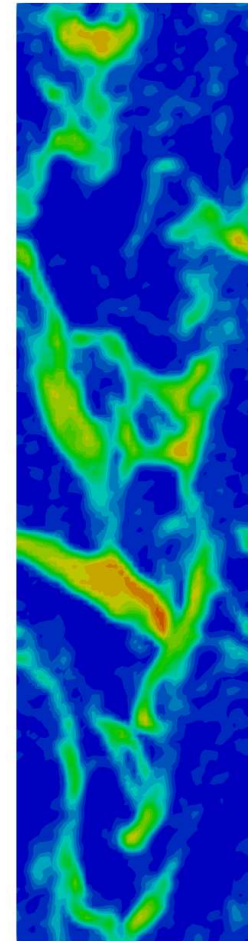
- Expensive, difficult & dirty
- indirect & noisy data from the plant

<https://www.gea.com/en/>

<https://burnertec.com/fcc-equipments/>

<https://www.industrialmeeting.club/food-processing-industry-plant-for-dry-mixed-products/>

- Modeling of gas-particle flows in **industrial-sized fluidized beds**
  - Typically, coarse-grid simulations using a “filtered” two-fluid model (fTFM)
- **fTFMs need sub-grid closure models** to approximate unresolved physical phenomena
  - Account for the effects of the inhomogeneous particle distribution
  - The drag force is essential for reliable prediction of flow behavior
- **Complexity increases** when considering **cohesive gas-particle** flows
  - Cohesive influence on the filtered drag force closure
  - Need for **faster (automated) closure development**

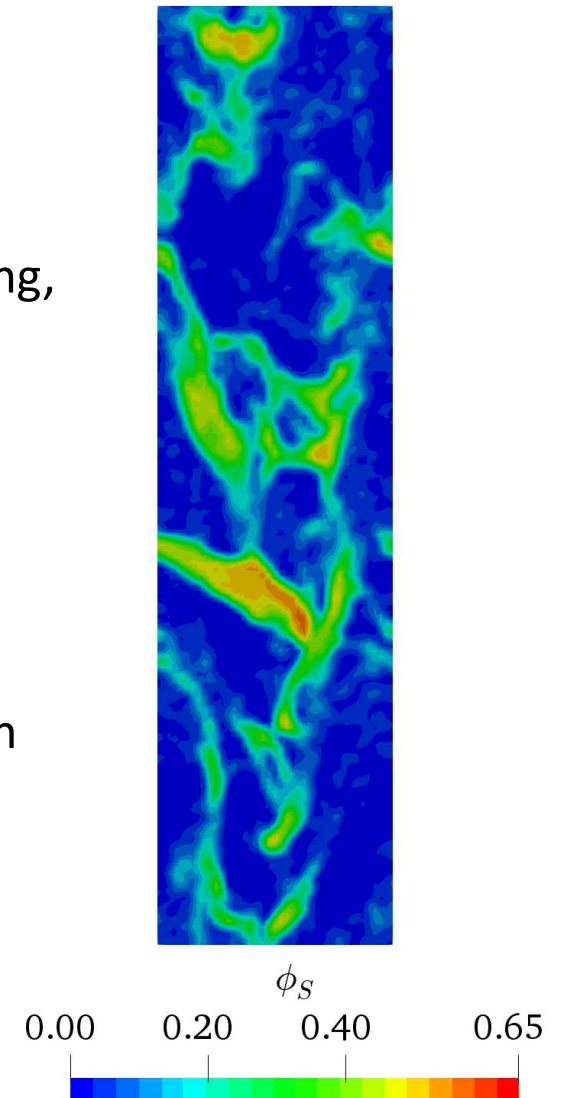


Sundaresan et al., AIChE J., 54, 2008. Igci & Sundaresan, Ind. Eng. Chem.

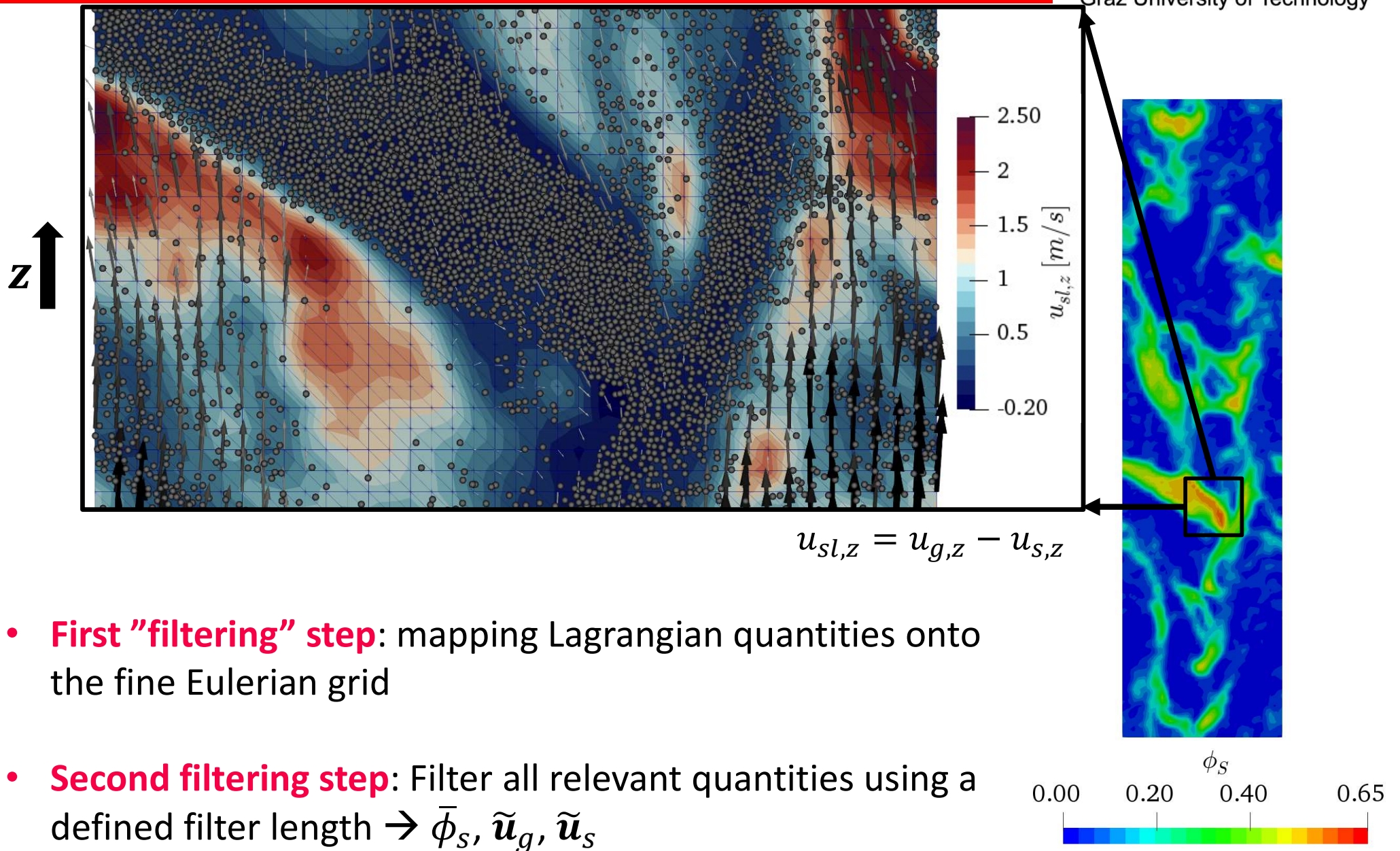
Res, 50, 2011; Yu et al., Powder Technology, 184, 2008

- Performing and then **filtering of “fine grid” simulations**
  - **Euler-Euler Approach**
    - Fluid and solid phase motion via continuum ansatz
    - complex particle-particle interactions (cohesion) challenging, but possible. **However, not the current focus...**
  - **Euler-Lagrange Approach**
    - Classical continuum-based ansatz only for fluid phase
    - Individual particle motion via Newton’s equation of motion
    - Large variety of models for **particle-particle** interactions
- ✓ **Our current focus**

**“ML-empowered” closure  
development**





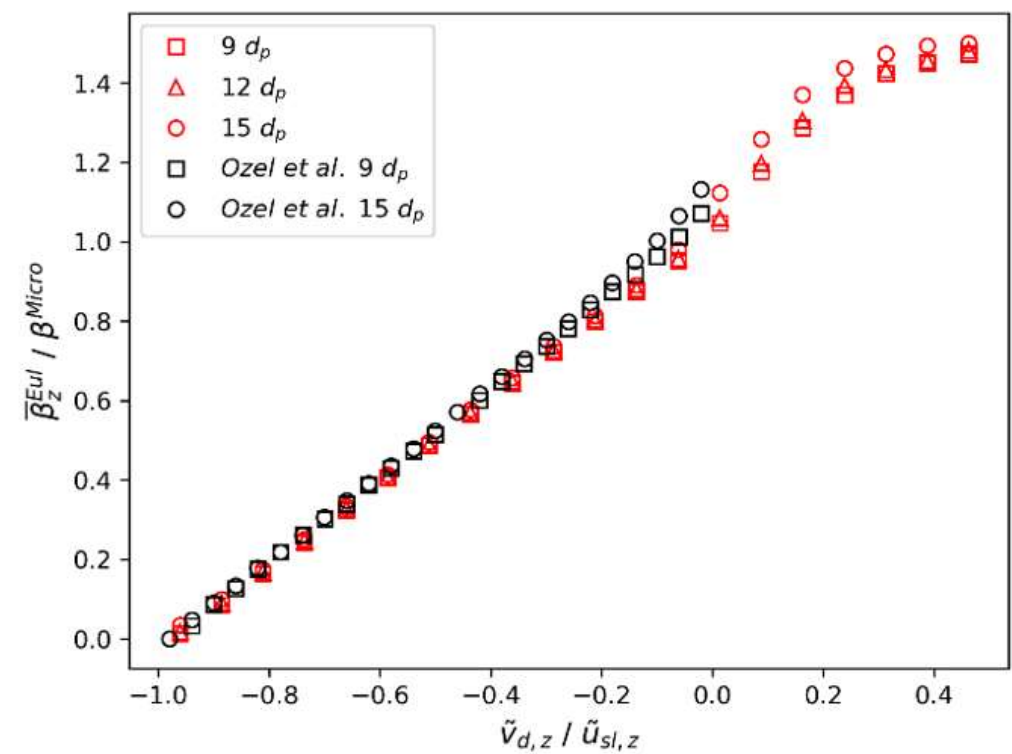
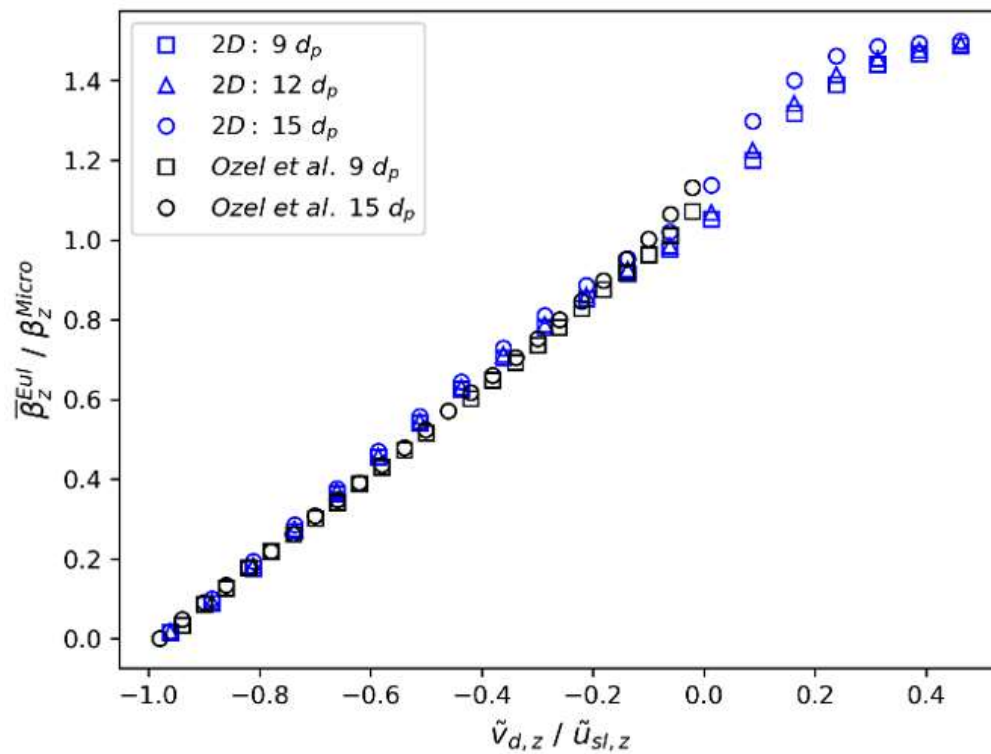


- Correction tensor  $\mathbf{H}_d = \frac{\text{drag in inhomogeneous state}}{\text{drag in hypothetical homogeneous state}}$
- This means it must fulfill the following properties:
  - $\mathbf{H}_d \rightarrow \mathbf{1}$  for sufficiently small filter sizes (i.e., “well-resolved” simulations)
  - $\mathbf{H}_d \rightarrow \mathbf{1}$  in the dilute limit (i.e., a single particle sedimenting at its terminal speed)
  - $\mathbf{H}_d \rightarrow \mathbf{1}$  in the dense limit (i.e., a particle suspension sedimenting at steady state)
- **Previous approach:** correlation functions based on just few features (“markers”):  $\bar{\phi}_s, \Delta_f, \tilde{\mathbf{u}}_{sl}$ :
  - Complex to build, limited applicability (poor training, not rigorous)
  - limited accuracy for larger filter lengths
- **Novel approach:** usage of **neural networks**
  - Fast, accurate & rigorous (many markers), and easy to integrate (e.g., Keras2CPP)
  - previously **only applied to dry systems**

- Keras<sup>®</sup> framework in Python
- DNNs with three hidden layers are optimal
- Rectifying Linear Unit (ReLU) activation function
- Training: mini-batch gradient descent method (MB size: 1024), Mean Absolute Error ( $MAE$ ) is the cost function
- Training time: 2D with 25 epochs → 0.5 hours, 3D with 50 epochs → 3.5 hours
- Hyperparameter search: up to 80 hrs in 3D



- „Validation“ with previous work



- Ansatz for the filtered drag force:  $\bar{\Phi}_{d,A} = \mathbf{H}_d \beta^{Micro} \tilde{\mathbf{u}}_{sl}$
- ...with the closure

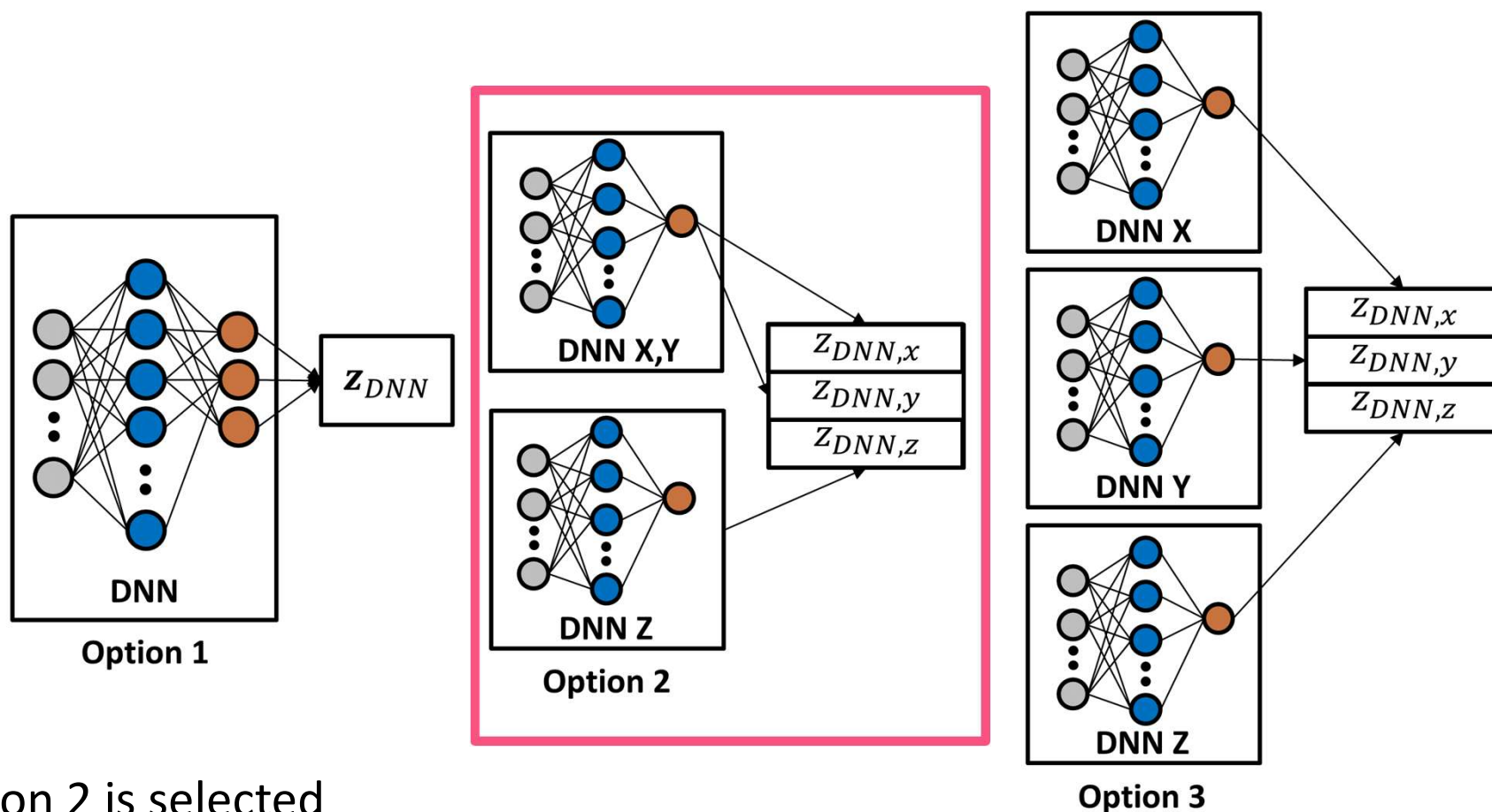
$$\mathbf{H}_d = \mathbf{1} + \frac{\phi_{s,max} u_t}{\bar{\phi}_s \tilde{u}_{sl,z}} \mathbf{z}$$

- The target and the prediction of the neural network is the **scaled drift velocity**

$$\mathbf{z} = \frac{\bar{\phi}_s \tilde{\mathbf{v}}_d}{\phi_{s,max} u_t}$$

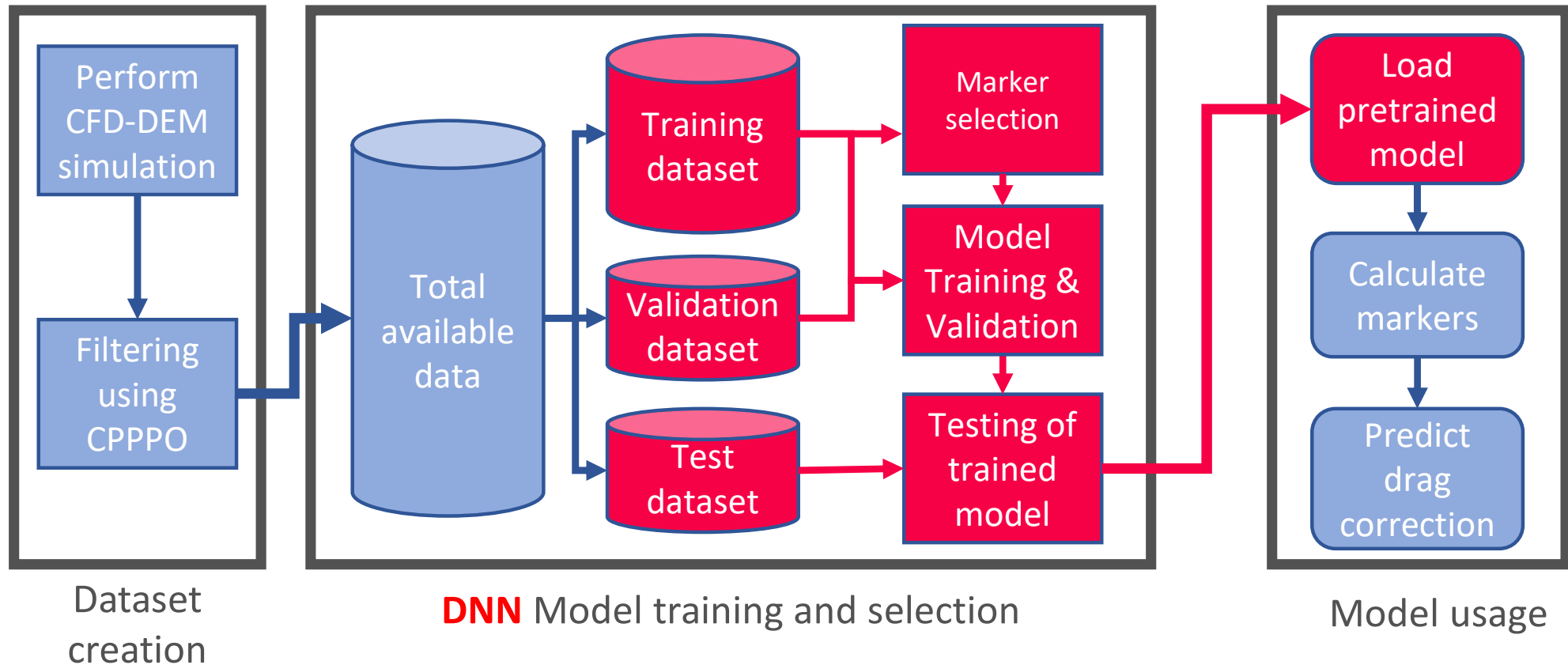
- For now, we consider all off-diagonal (“lift like”) values of  $\mathbf{H}_d$  to be zero. However, diagonal elements of  $\mathbf{H}_d$  are not identical (**anisotropic correction**)

- Prediction based on vector-valued markers must ensure Galilean invariance
- Three basic options to formulate a drag correction



- Option 2 is selected
  - An internal coordinate system, that respects rotational invariance, can be intuitively spanned





- Markers (“**Features**”)

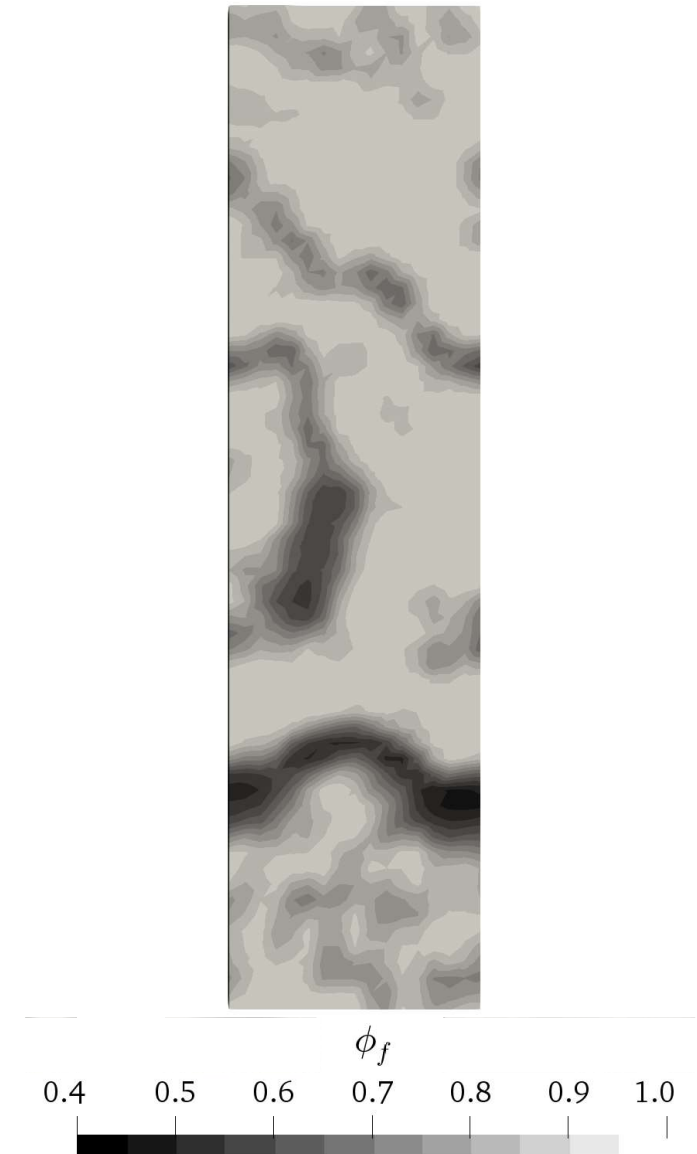
$$\psi = \left( \frac{1}{\Delta_f^*}, \frac{\bar{\phi}_s}{\phi_{s,max}}, \frac{\tilde{\mathbf{u}}_{sl}}{u_t}, \overline{\nabla p_z^*}, Bo, \overline{\dot{\gamma}_{sl}^*}, \overline{\dot{\gamma}_s^*}, \frac{\|\tilde{\mathbf{u}}_{sl,xy}\|}{u_t} \right)$$

- All markers min/max normalized prior to usage

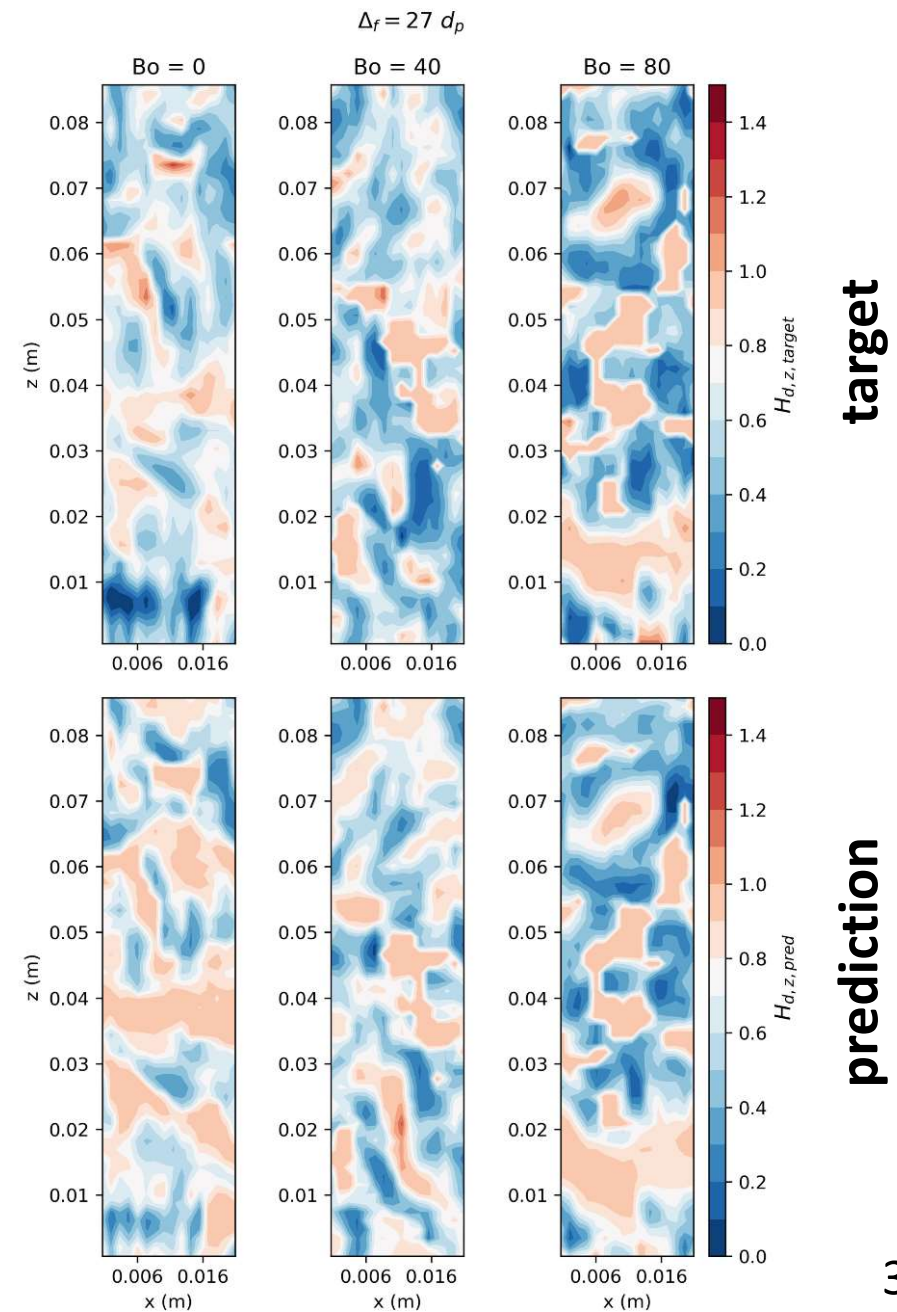
$$\alpha = 3$$

- Pseudo **2D & 3D CFD-DEM** simulations
  - Domain size is  $16 \Delta_G \times 2$  (or  $16$ )  $\Delta_G \times 64 \Delta_G$
  - Total particle volume fraction  $\phi_{s,tot} = 0.10$
  - Filter sizes are:  $3 \Delta_G, 4 \Delta_G, 5 \Delta_G$
- Scaling of **coarse graining parameters** following Tausendschön et al.
- Dry to **highly cohesive** systems (cohesion from liquid bridges: capillary & viscous)

	$\alpha = 3$
$d_P [\mu m]$	450
$\Delta_G [\mu m]$	1,350
$N_{prime}$	285,147
Parcels	10,561
$Bo$	0 – 80



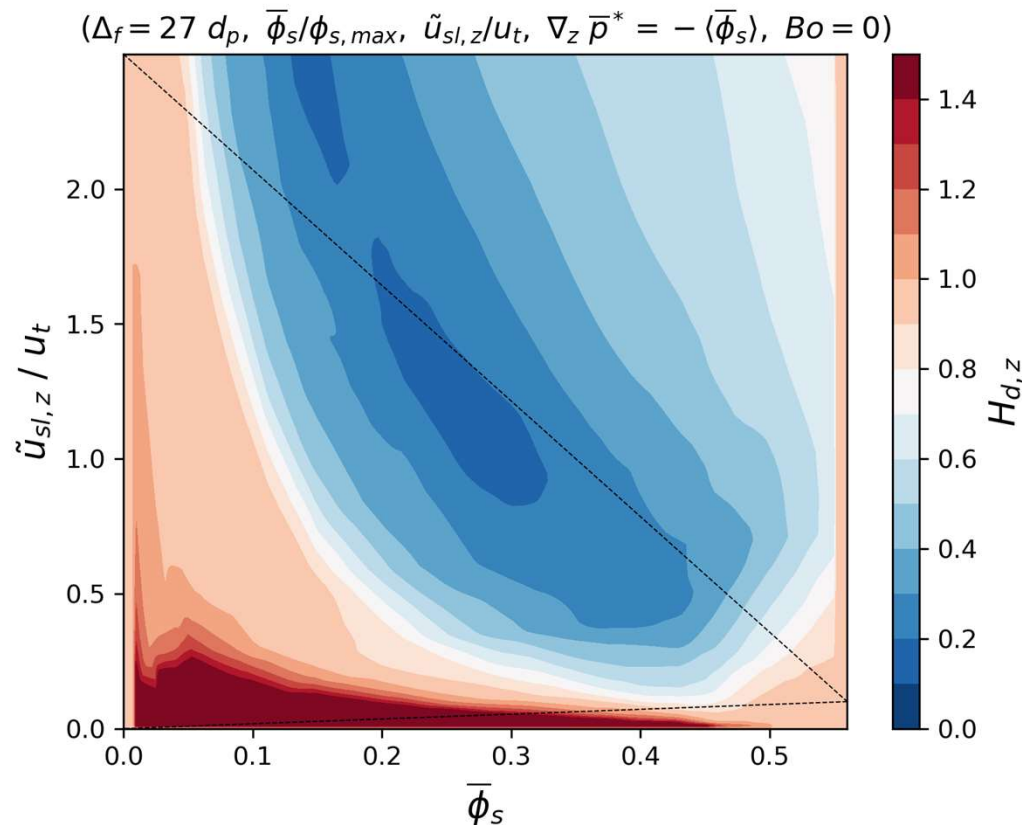
- 2D & 3D, gravitational direction only
- Spatial distribution of the drag correction functions is sensitive to Bond number (“diffuse” versus “focused” for low and high Bond, respectively)
- Reasonable agreement, except for “extreme” regions (e.g., local maxima in the  $H_d$  field)



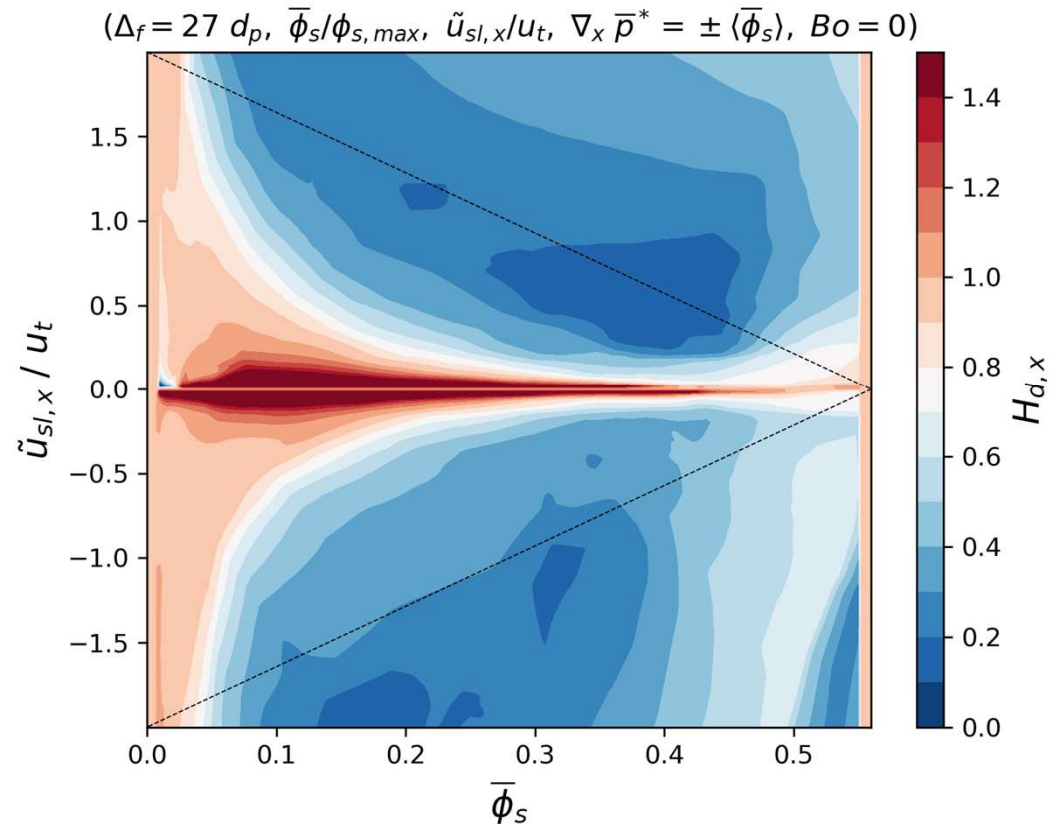


- Distribution of correction values in  $\bar{\phi}_s - \tilde{u}_{sl}/u_t$  plane

## Gravitational direction



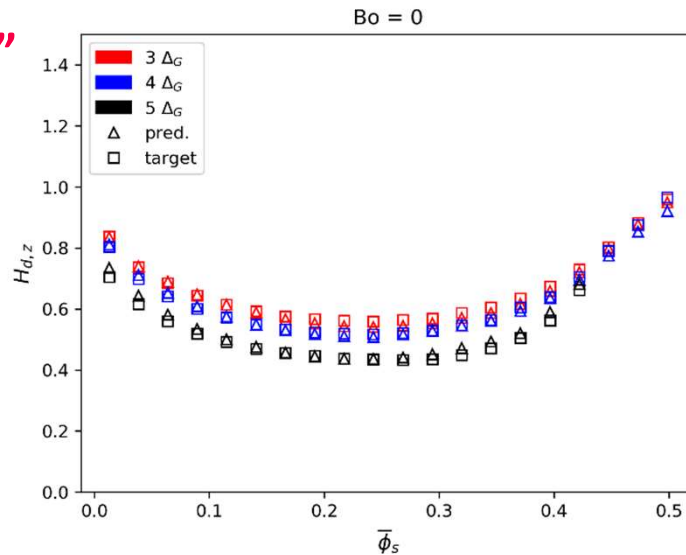
## Lateral direction



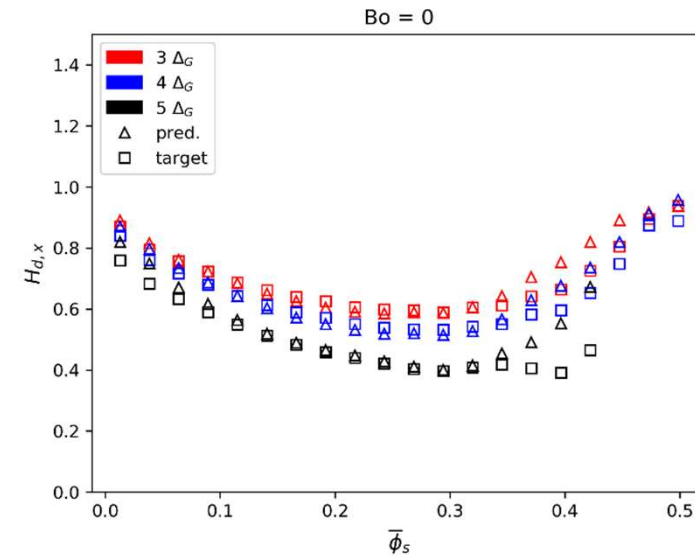
- Significant and non-trivial change with Bond number

“bin-  
averaged”  
data  
(non-  
cohesive)

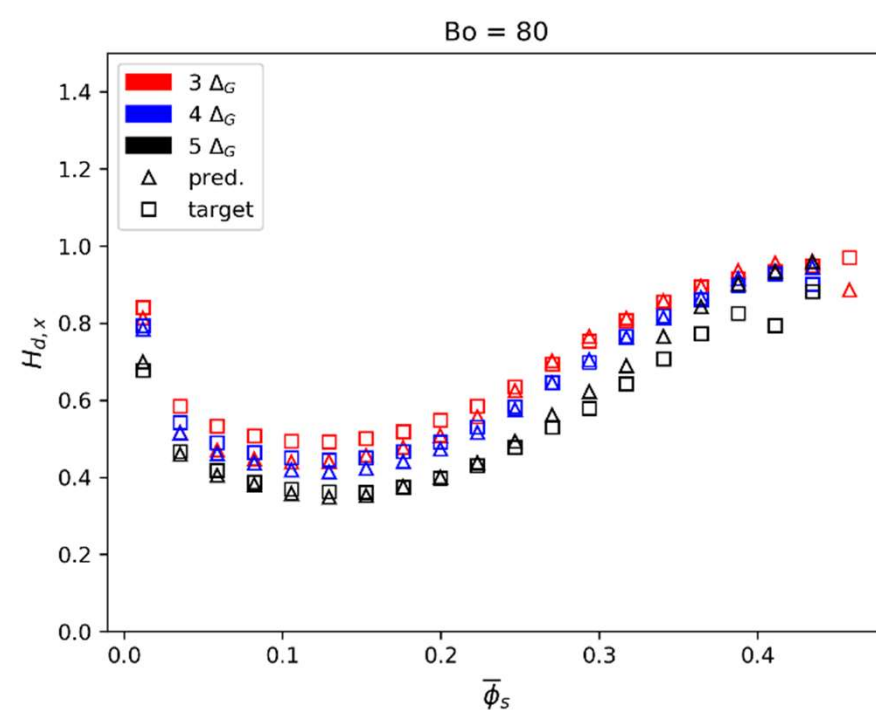
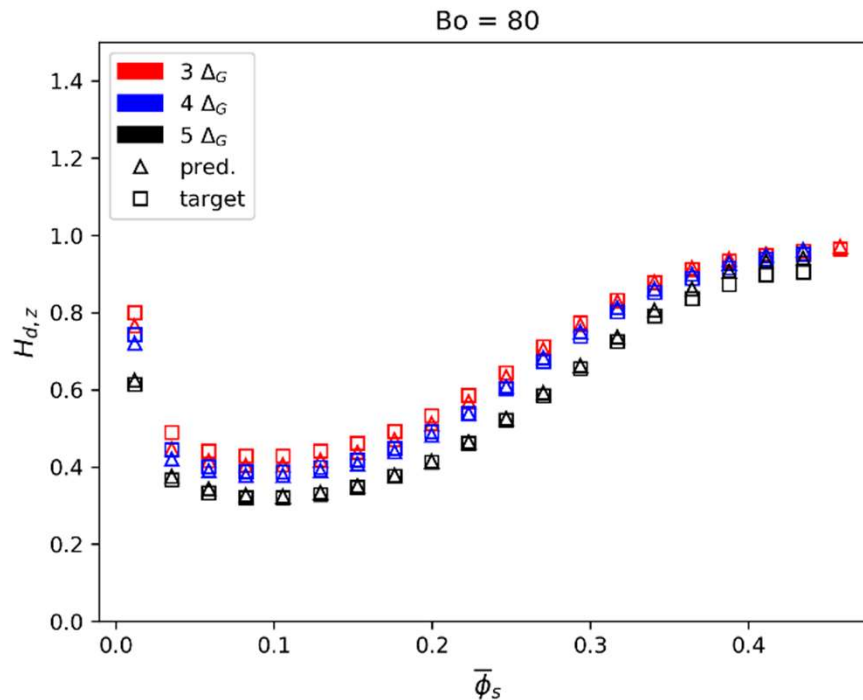
gravitational direction



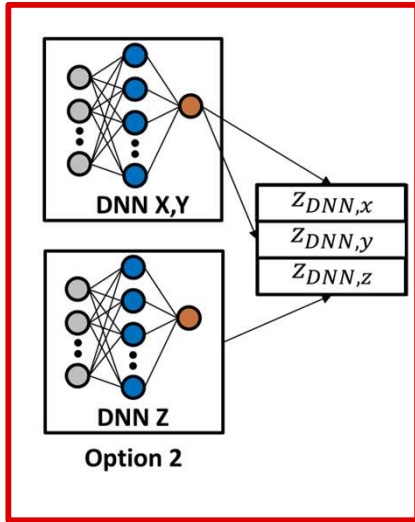
lateral direction



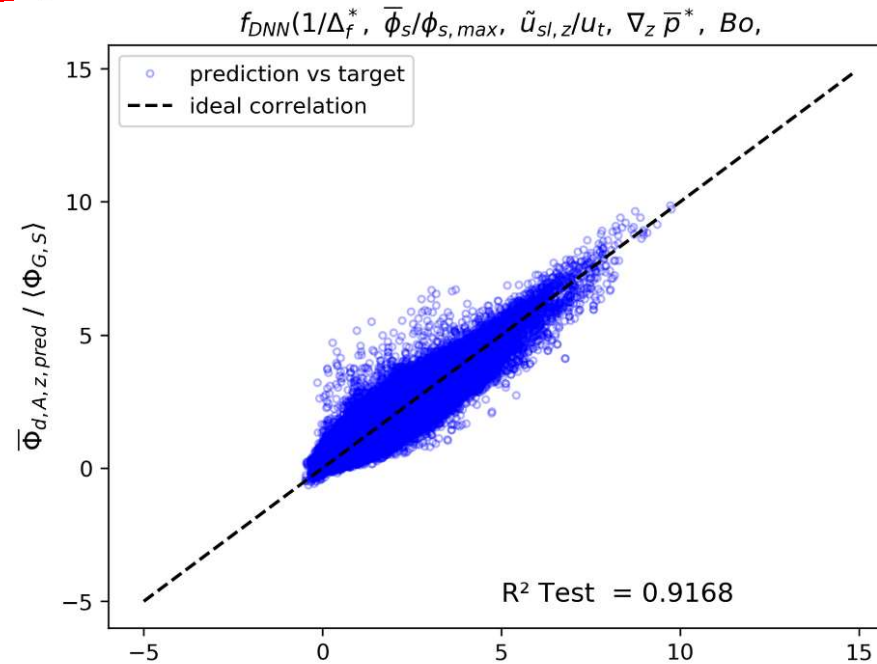
cohesive



# Workflows & ML::Need4Speed::Result VIII

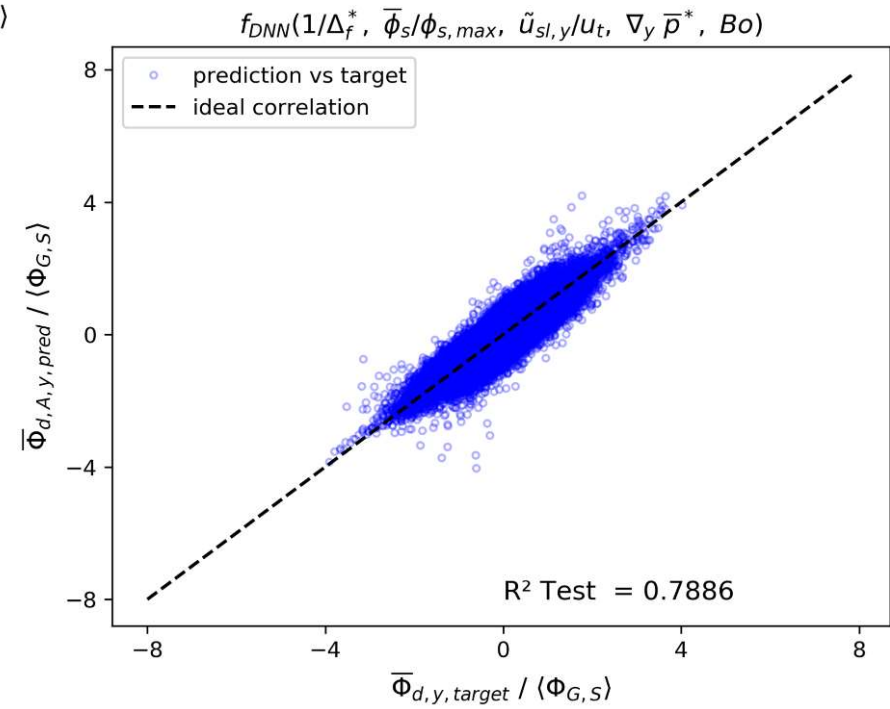
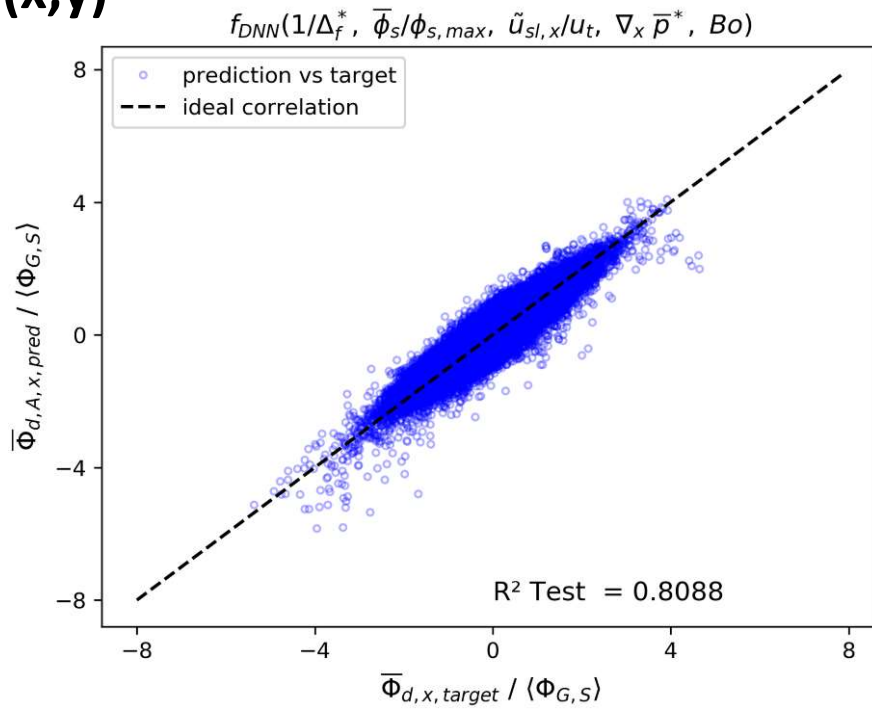


lateral directions  
(x,y)



Individual samples  
("raw filtered data")

gravitational  
direction (z)





- The “**chicken crossing a street** challenge”: calibration has become a standard approach to make simulations “more realistic”
  - Sequential direct calibration approach (Aspherix® calibration)
  - Response surfaces: Superimposing the results of multiple numerically replicated experiments for a range of parameters
- **Common challenges**
  - lack of **graphical calibration workflows, or even the workflow**
  - absence of a **clear & FAIR data handling strategy**

Irrespective of the calibration method, the workflow needs to handle a huge amount of data

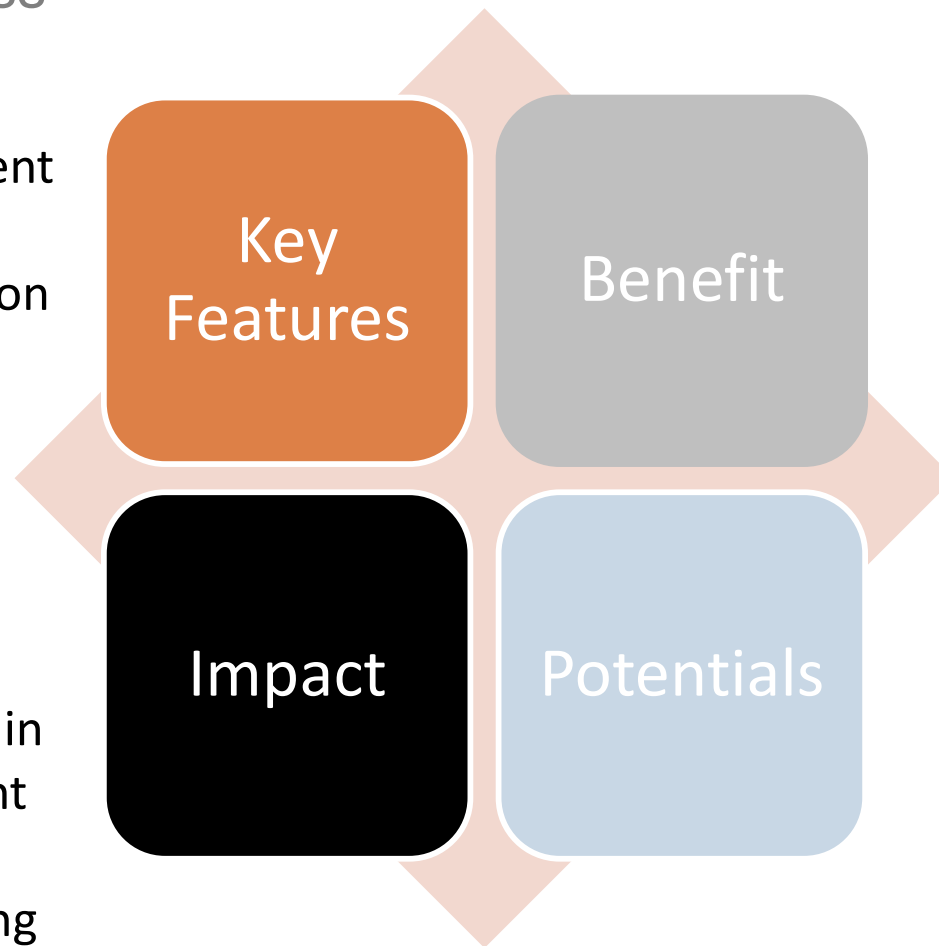
Coetzee, Powder Technology, 2017. Roessler et al, Powder Technology, 2019. Do et al, advanced powder technology, 2018. Richter et al, Powder Technology, 2020

## DEMvironment

A workflow environment for data management of DEM parameter calibration process

- Data management
- Guide for experiment selection
- Steers the calibration workflow

- Speeding up the process
- Increase efficiency in model development
- Increased collaboration among researchers and practitioners



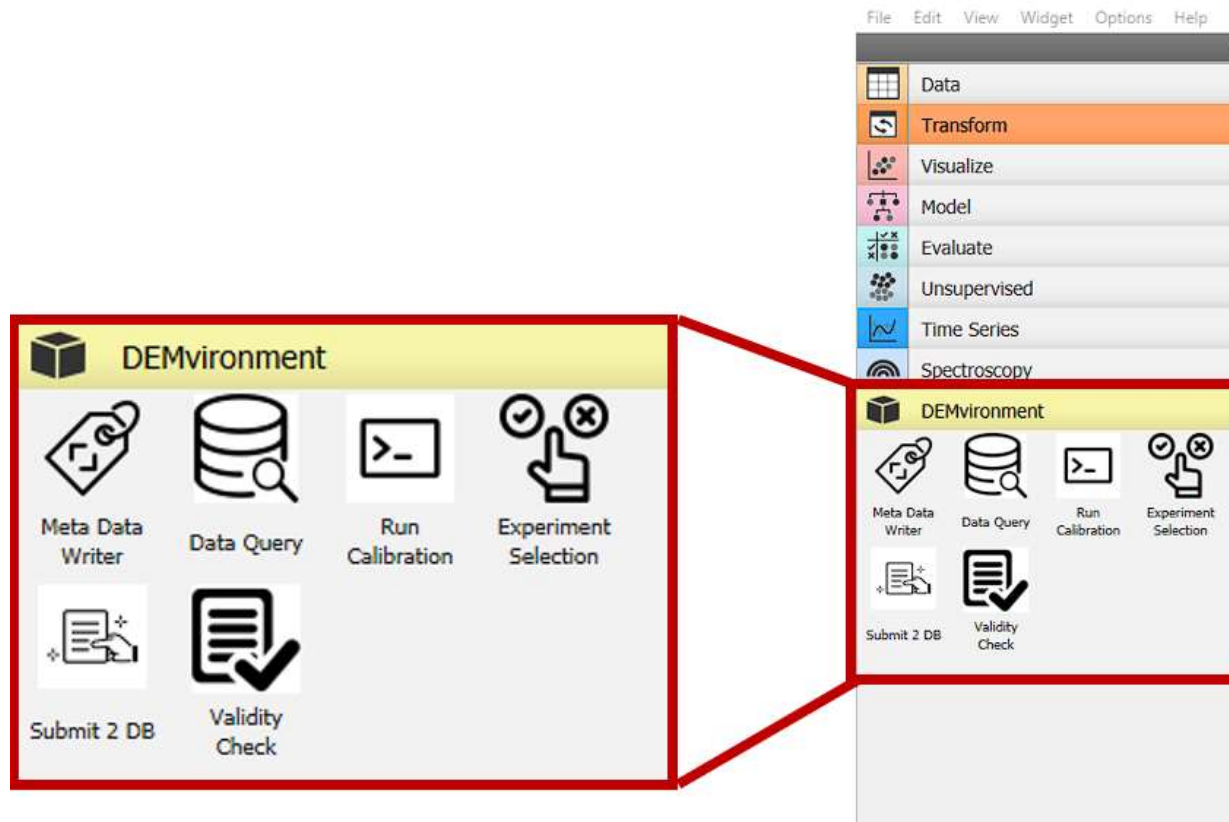
- User-friendly interface
- Automated parameter calibration
- Reproducibility of the process
- Open source
- Allows steering more sophisticated ML algorithms
- Can be applied to other particle simulation techniques

## DEMvironment interface

...soon available in Orange3

orange  
DATA MINING  
FRUITFUL&FUN

python™



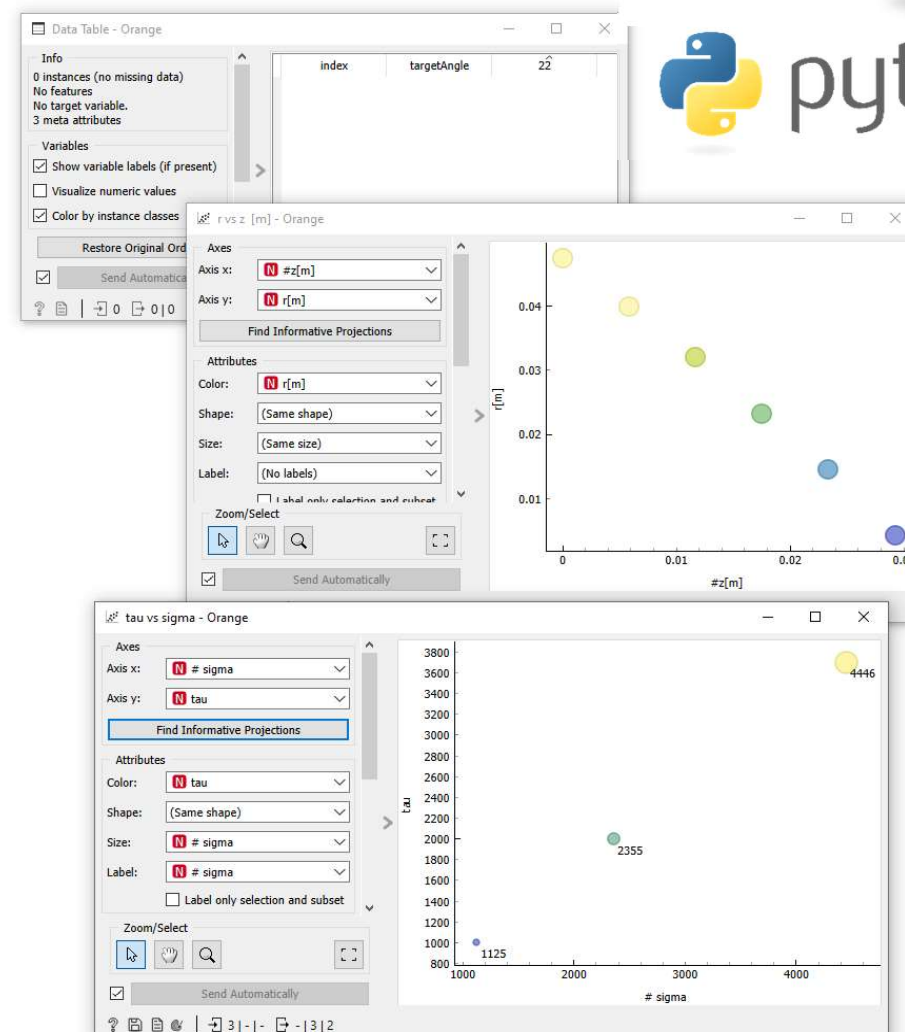
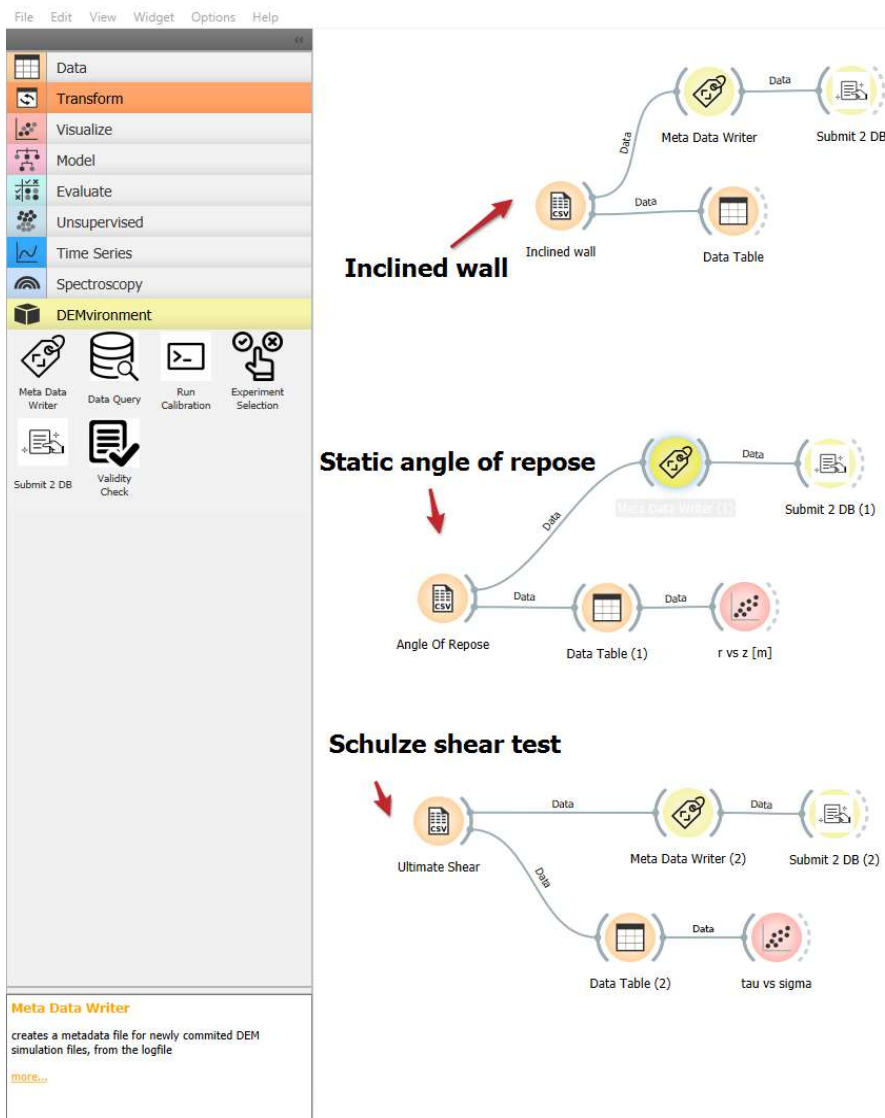
<https://n-ghods.github.io/workflowenv>

## DEMvironment interface

...soon available in Orange3

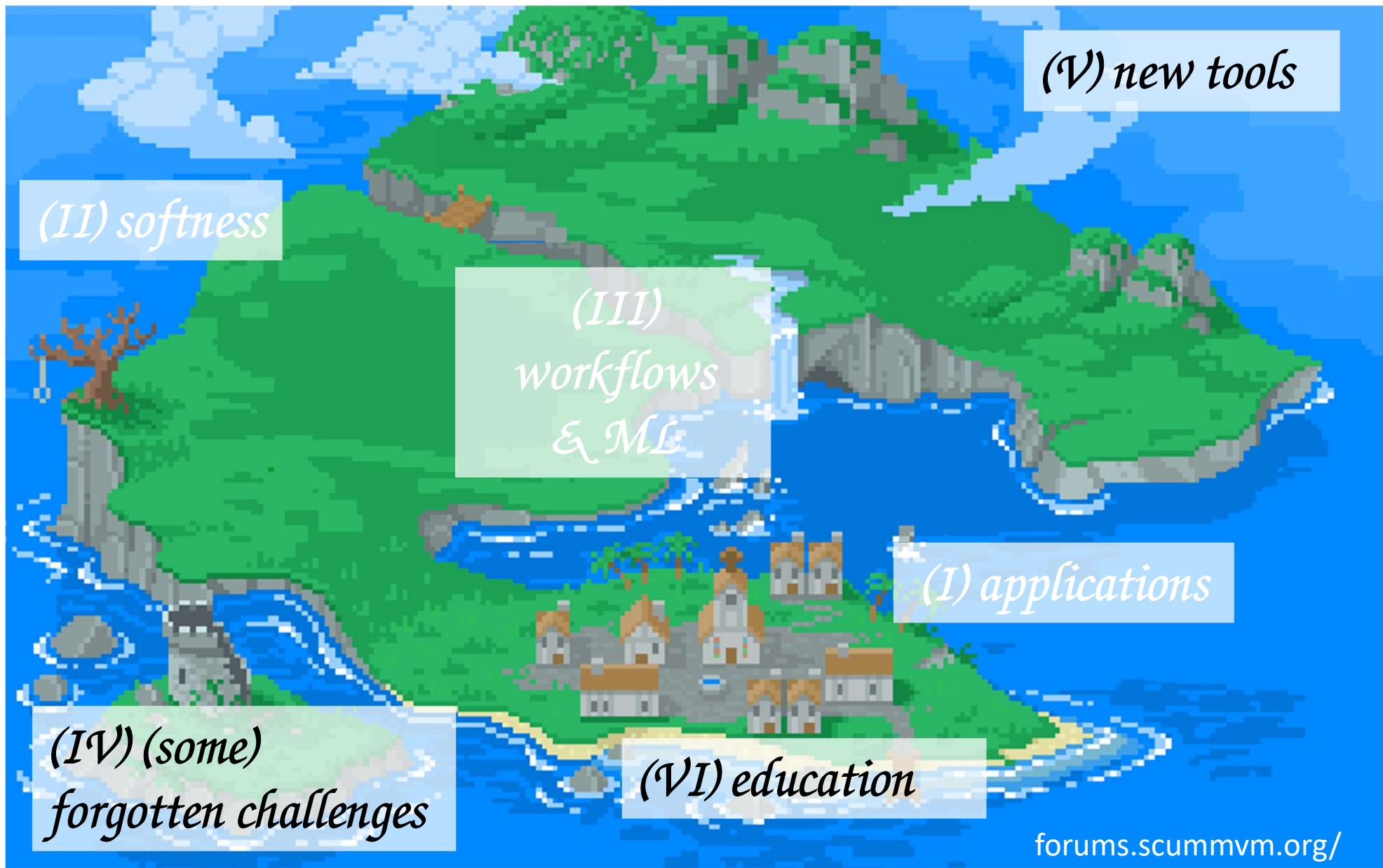
orange  
DATA MINING  
FRUITFUL&FUN

python™





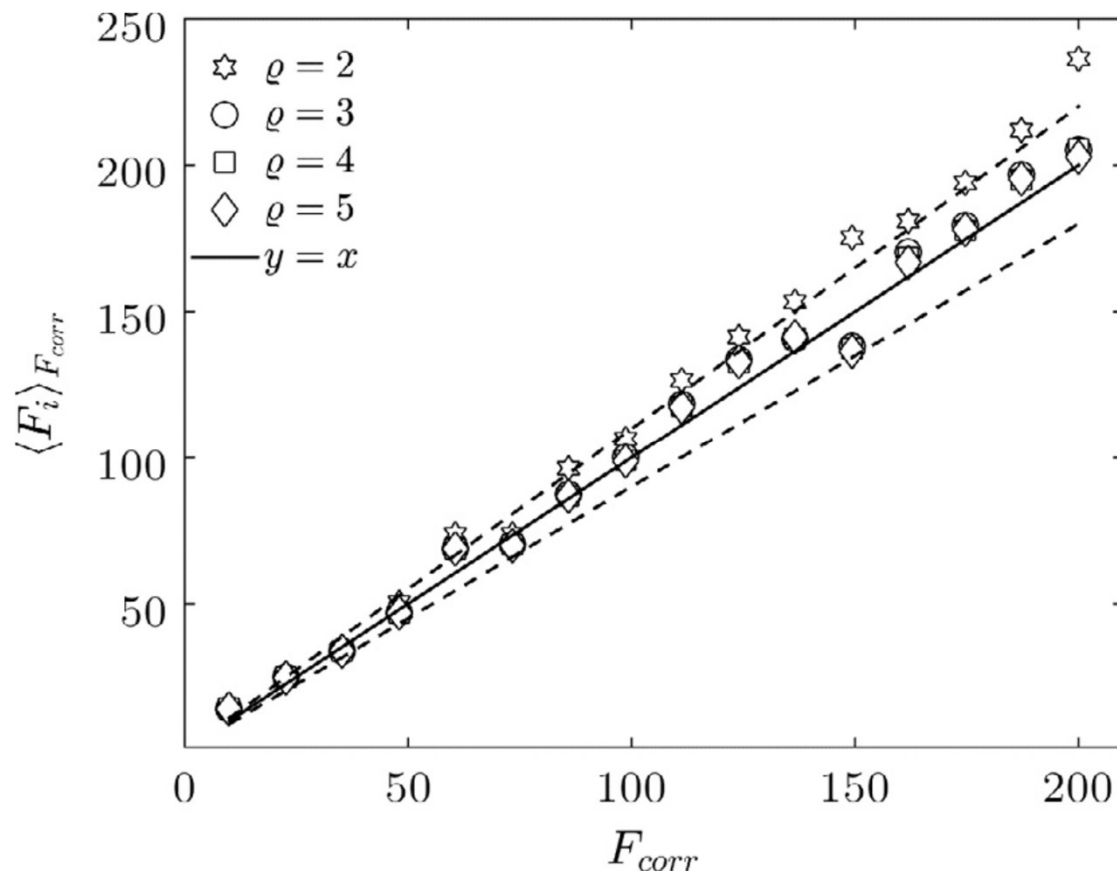
# Overview



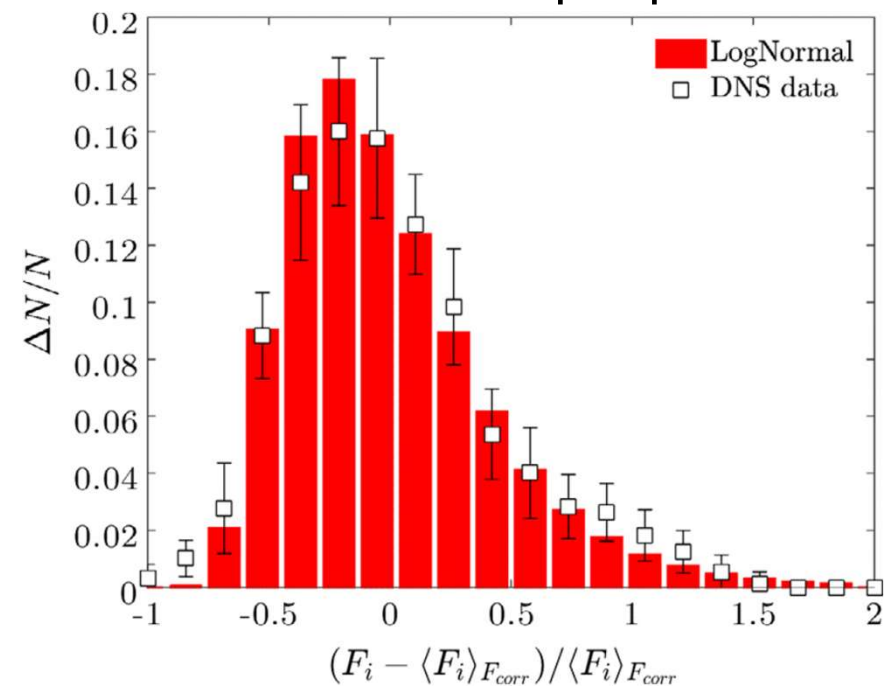
## Let us reflect...

What would we need to go “beyond” current CFD-DEM capabilities?

Fluid-particle drag (and Nusselt number) is okay „on average“....



....but there is a wide distribution on a per-particle!

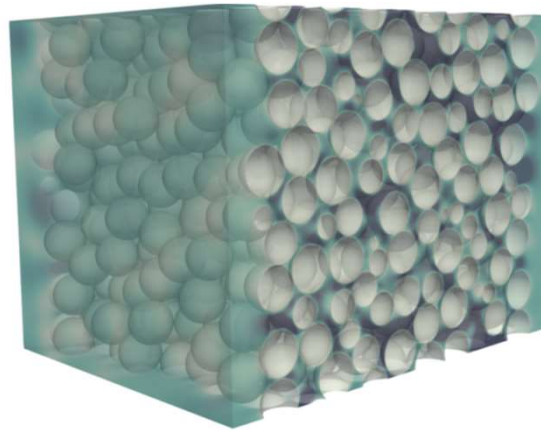


Municchi & Radl, Int J Heat Mass Transfer, 2017

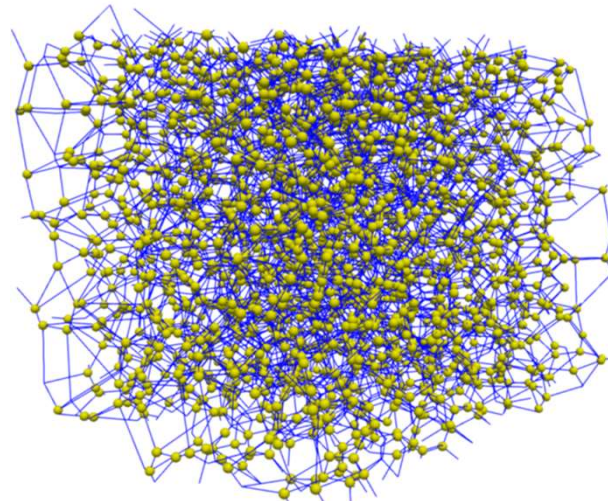
## Let us reflect...

What would we need to go “beyond” current CFD-DEM capabilities?

Possible solution:  
use a pore network  
model to improve  
flow prediction...



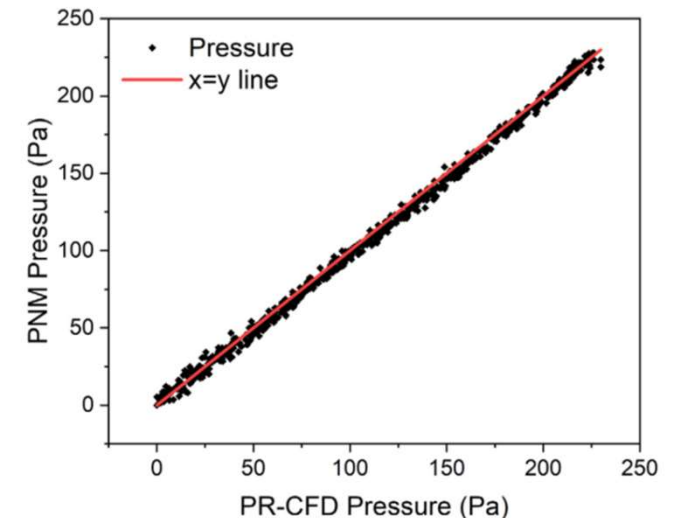
(a)



(b)

Morimoto et al,  
Computers &  
Geotechnics, 2022

....with recent success! But  
what is the computational cost?  
Is their calibration universal?



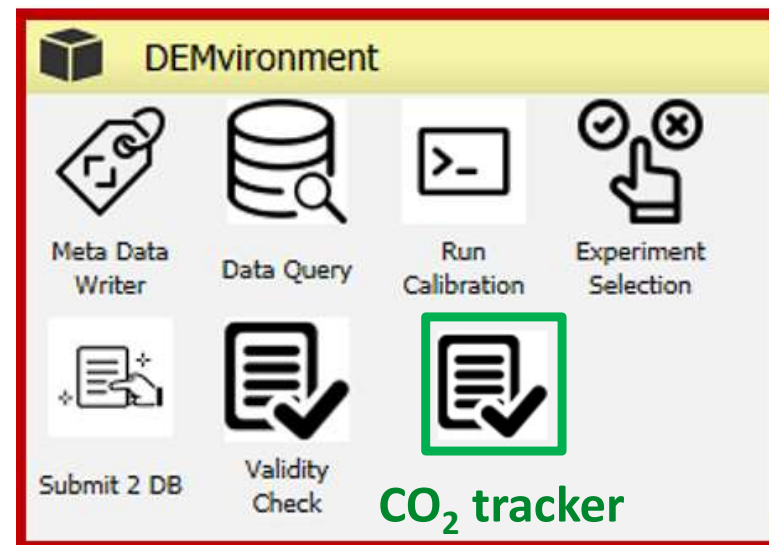
Fathiganjehlou et al.,  
Chem Eng Sci, 2023

## What should happen next...

...tools and their upgrades

- CPPPO's general interface with lagrangian (DEM) data
- Filtering over a fixed number of particles (instead of a fixed region size)
- More filter kernels
- Integration of CO<sub>2</sub> tracker into workflow tool (eco sweet spot of modeling effort)

[https://yopad.eu/p/SoSe23\\_seminarHannover](https://yopad.eu/p/SoSe23_seminarHannover)

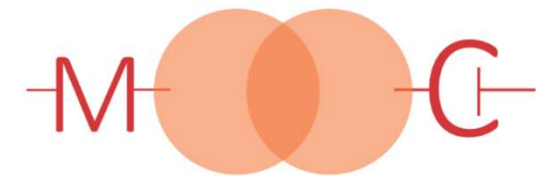




- **Start slow and simple** (analytics first, then simulation; Python first, then C++)
- **Use existing tools** (Orange3, then KERAS/TensorFlow)
- **respect FAIR data management** principles (because only complete data is useful data)
- **Preservation of knowledge** requires a dedicated work package



**Grants** 813202  
& 812638

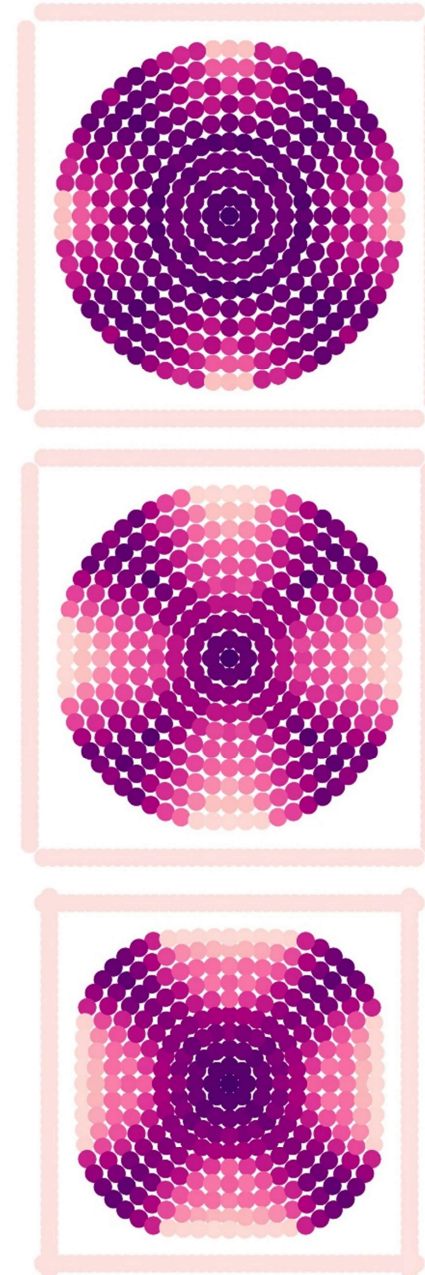


The  
**Discrete Element Method**

<https://imoox.at/course/dem>

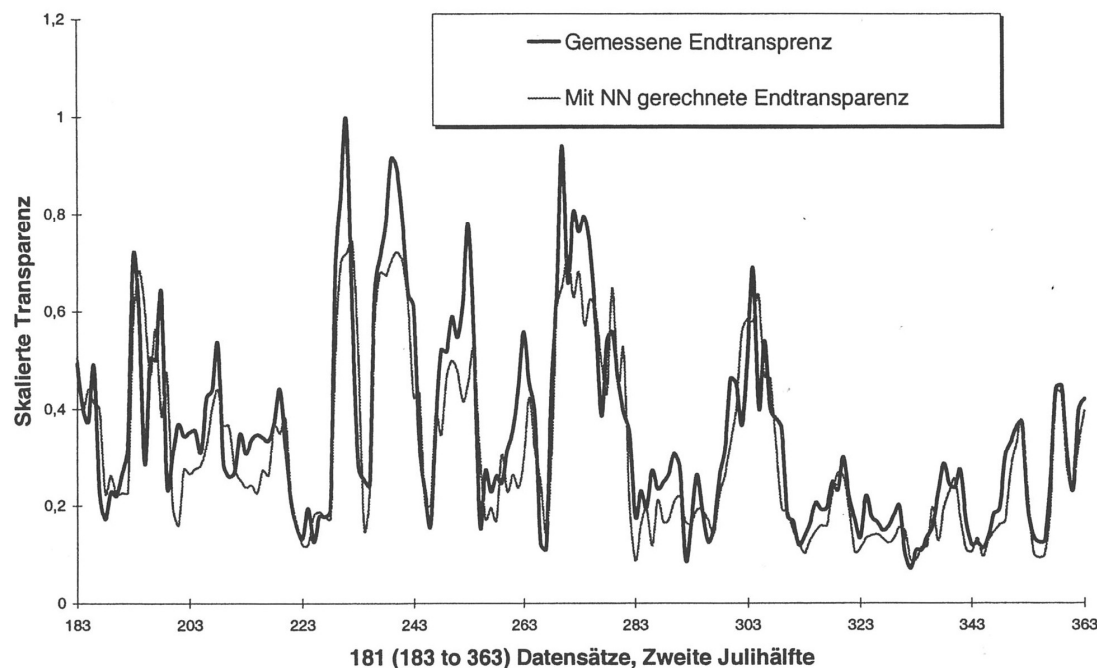
**MOOC starting in fall 2023**

- **Softness** must be seen in relative terms (pressure/elasticity ratio)
- **Various approaches** exist, simple extension to DEM possible (currently only spheres)
- **Poisson ratio** becomes an additional influence parameter
- Full **flexibility** (SPH, bonded particles, FEM) comes with **significant computational cost**
- advanced **MC DEM together with calibration** a promising strategy



# Conclusion II

- **(Cohesive) sedimenting suspensions** are our daily business since many decades. Cohesion may require a **paradigm shift** to a “closure database” approach
- Reading old PhD thesis can give **inspiration** for **new features to be used in ML** (data @  $t-\Delta t$ , smart NN testing).



Fuchs, Diss. TU Graz, 1999



- **Anisotropy** of drag and stress closures must be considered. “Hand fitting” of this **set of 5 marker closures** would be **extremely time consuming** → **central motivation for usage of DNNs**.
- Huge **unexploited potential** when considering individual samples of the filtered drag force. Reasons: fundamental assumption  $\bar{\Phi}_{d,A} = \mathbf{H}_d \beta^{Micro} \tilde{\mathbf{u}}_{sl}$ .
- Drag corrections are **stronger** (i.e., lower drag forces) **for cohesive systems**. Speculated reason: **more compact clusters for high Bo**.
- Options for future work
  - DNN-based closure for **meso-scale stresses**. A posteriori testing of the drag correction models in a **ftFM simulation framework**
  - **“Free” (tabulated, NN-based) force models** for **coarse graining** cohesive powder models



Beyond classical CFD-DEM

# Forgotten Challenges and New Tools

# Thank you



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